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(54) **CATALYTIC HYDROFORMYLATION OF VINYL TERMINATED POLYOLEFINS**

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24, 2012.

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C08F 8/06 (2006.01)
C08F 210/06 (2006.01)
C08F 210/08 (2006.01)
C08F 210/14 (2006.01)
C08F 110/06 (2006.01)
C08F 8/00 (2006.01)

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C08F 210/06 (2013.01); **C08F 210/08**
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(58) **Field of Classification Search**

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C08F 210/14; **C08F 8/00**; **C08F 8/06**; **C08F**
8/10

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526/348.5, **348.6**, **351**

See application file for complete search history.

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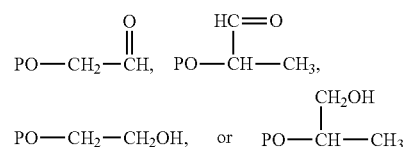
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(57) **ABSTRACT**

This invention relates to a polyolefin composition comprising one or more of the following formulae:



wherein the PO is the residual portion of a vinyl terminated macromonomer (VTM) having had a terminal unsaturated carbon of an allylic chain and a vinyl carbon adjacent to the terminal unsaturated carbon; and wherein the VTM is preferably a vinyl terminated polymer having greater than 30% allyl chain ends with an Mn of greater than 10,000.

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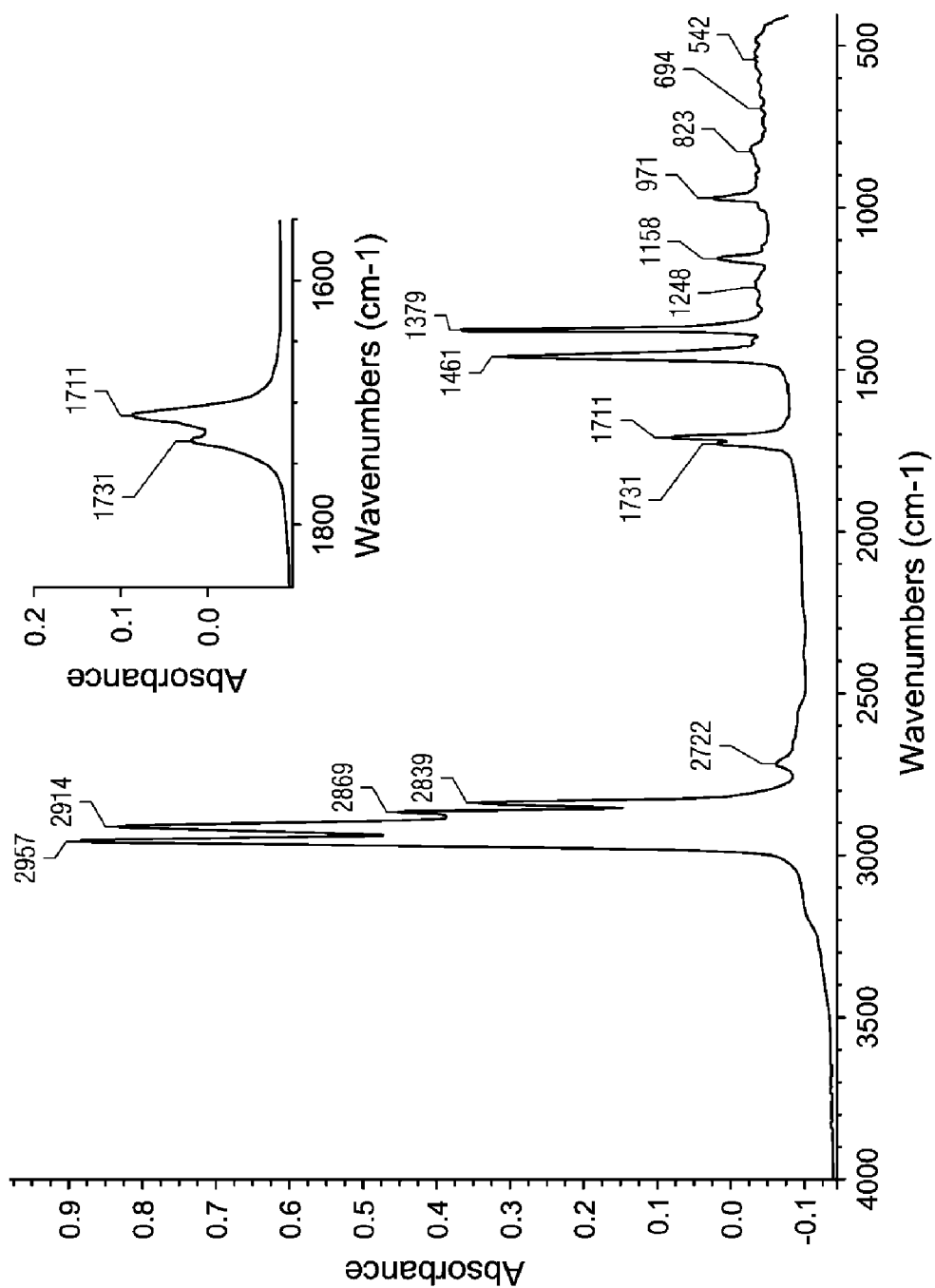


FIG. 1

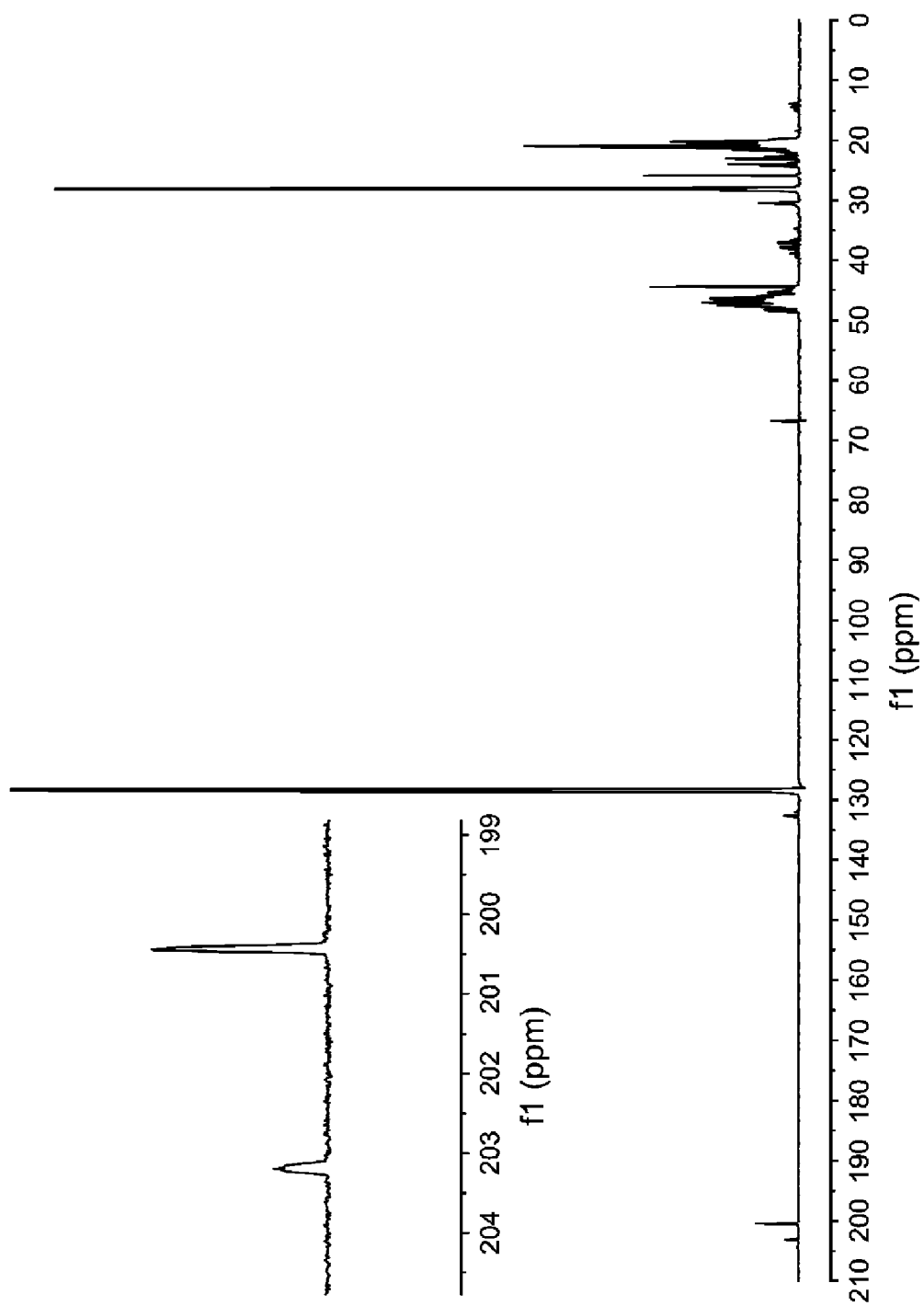


FIG. 2

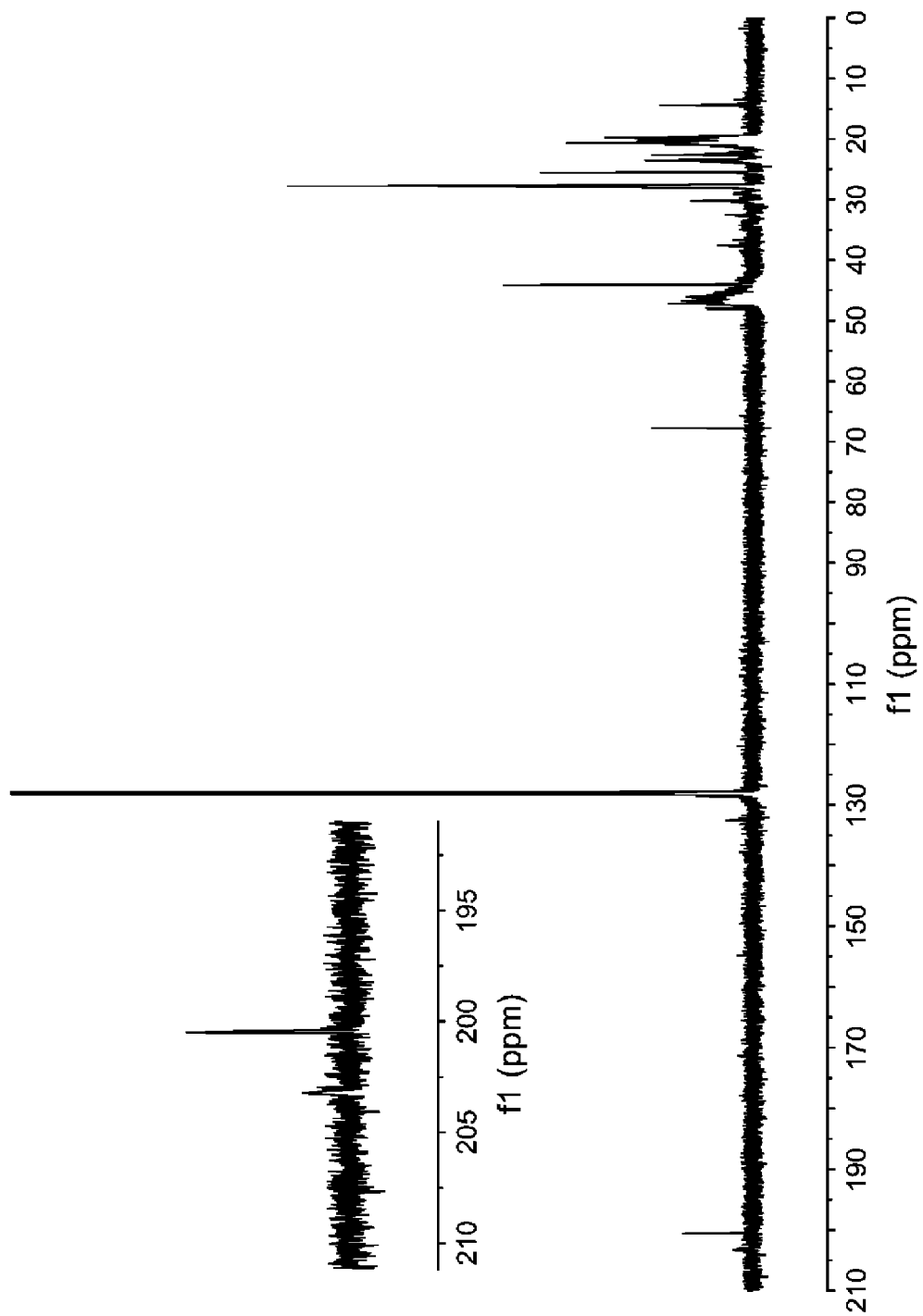
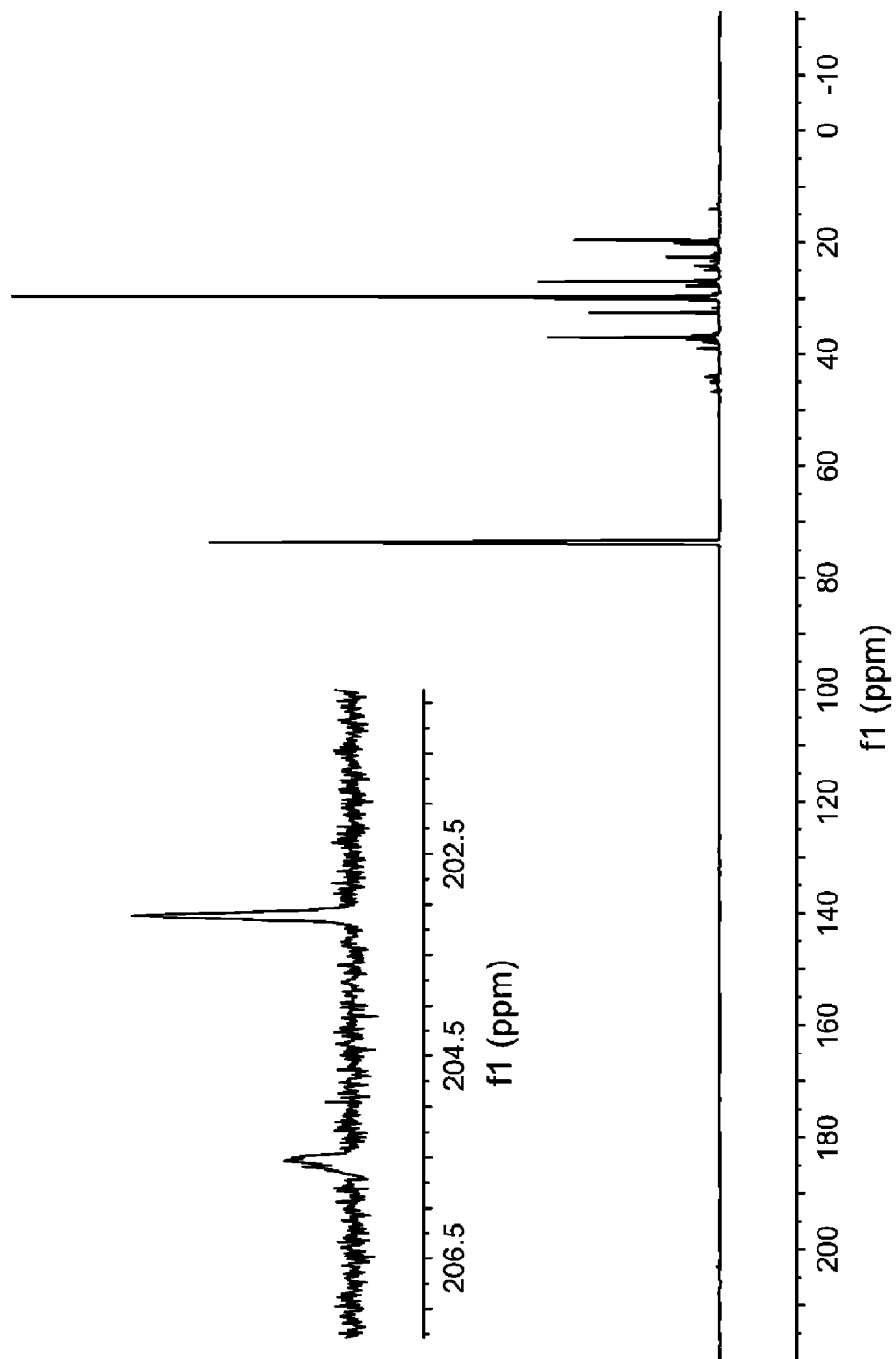


FIG. 3



f1 (ppm)

FIG. 4

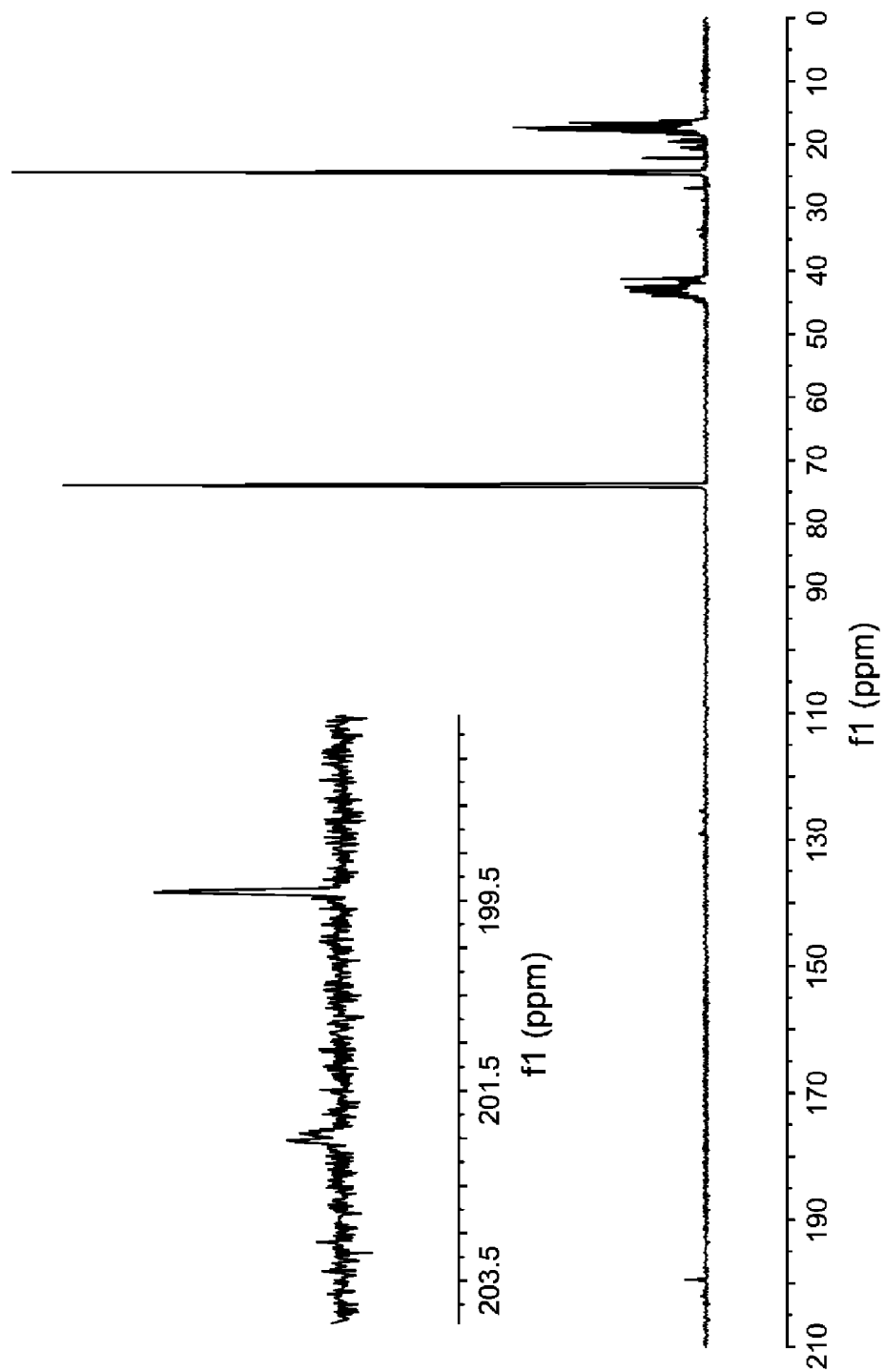


FIG. 5

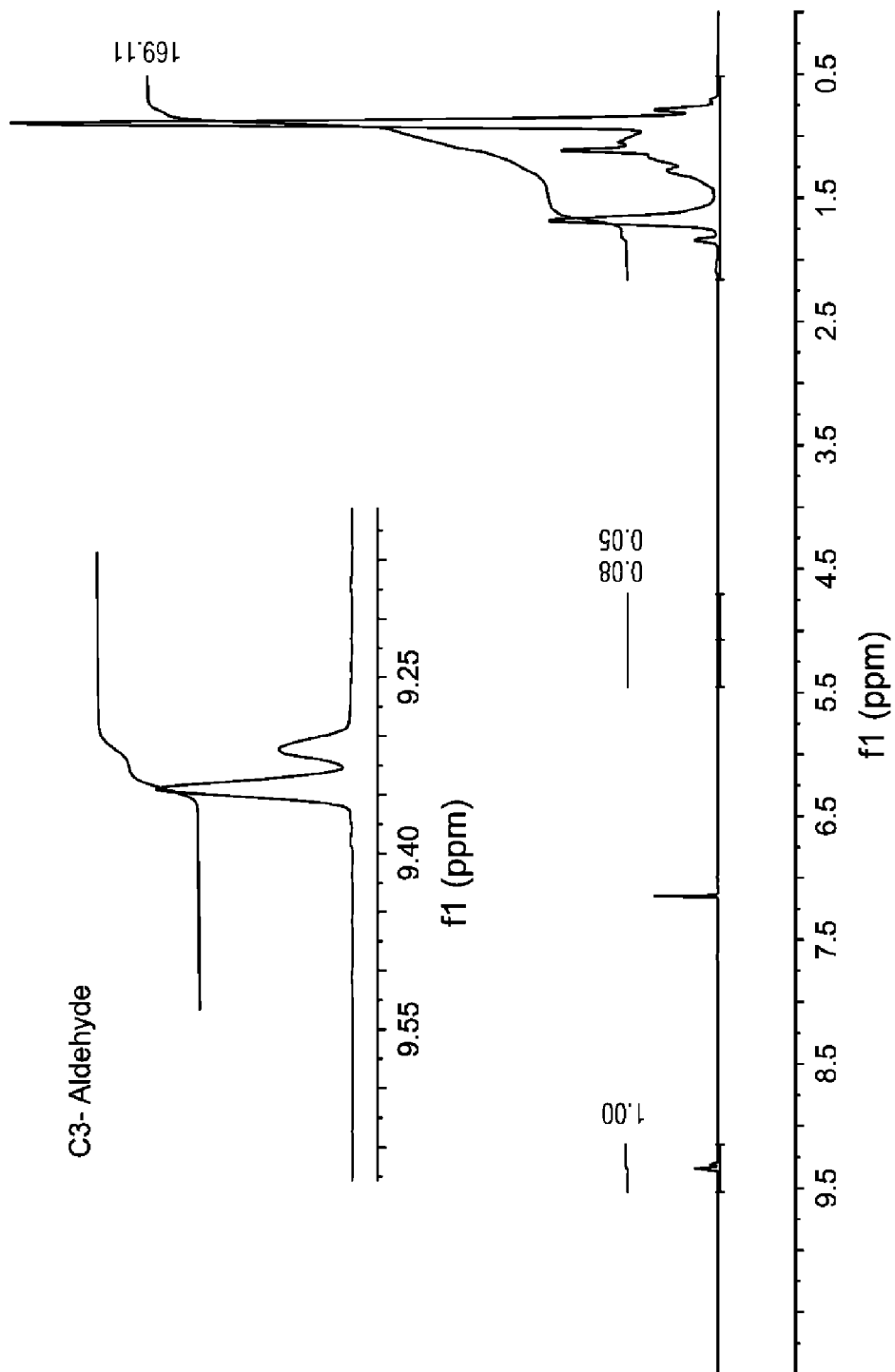


FIG. 6

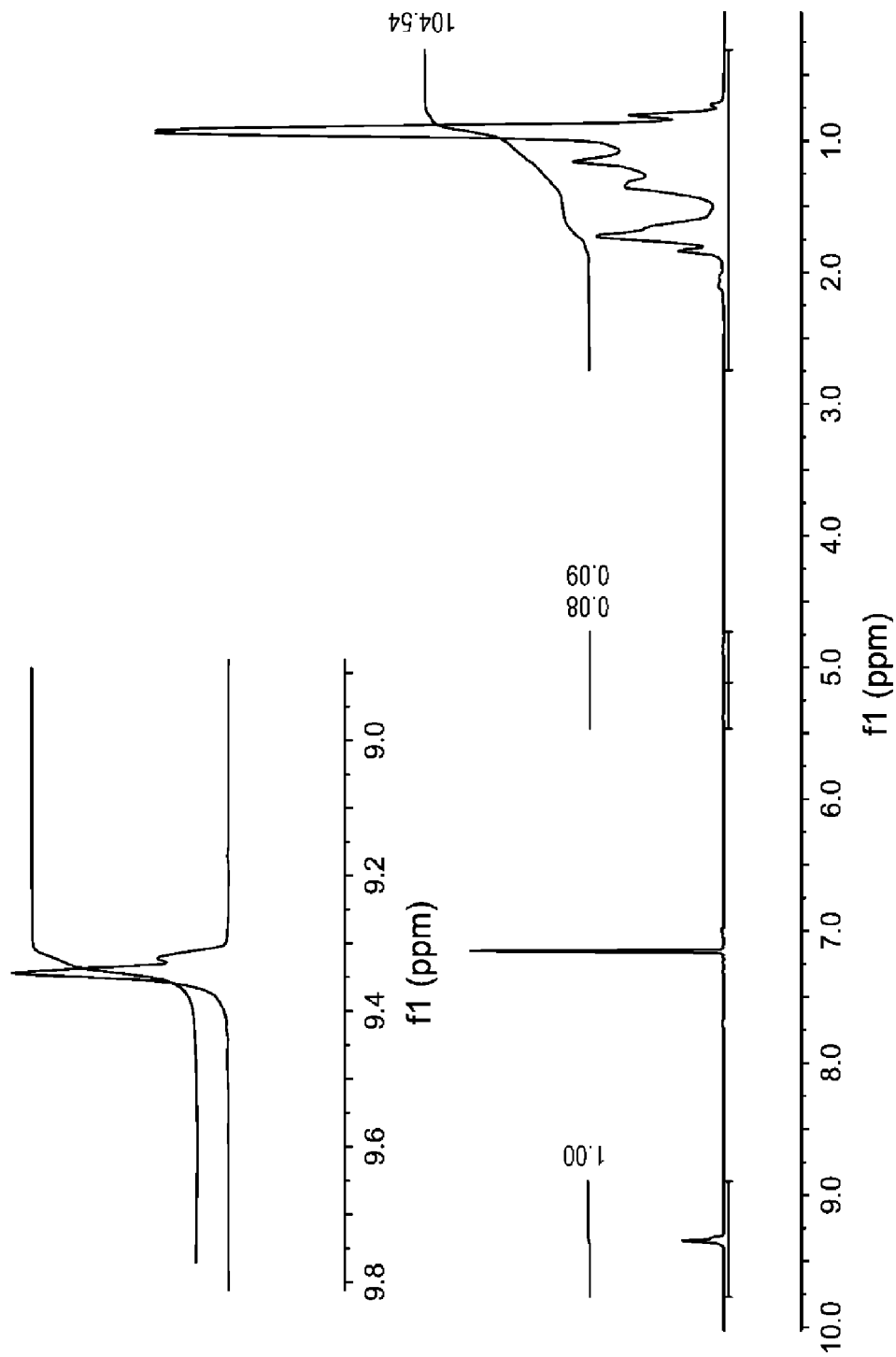


FIG. 7

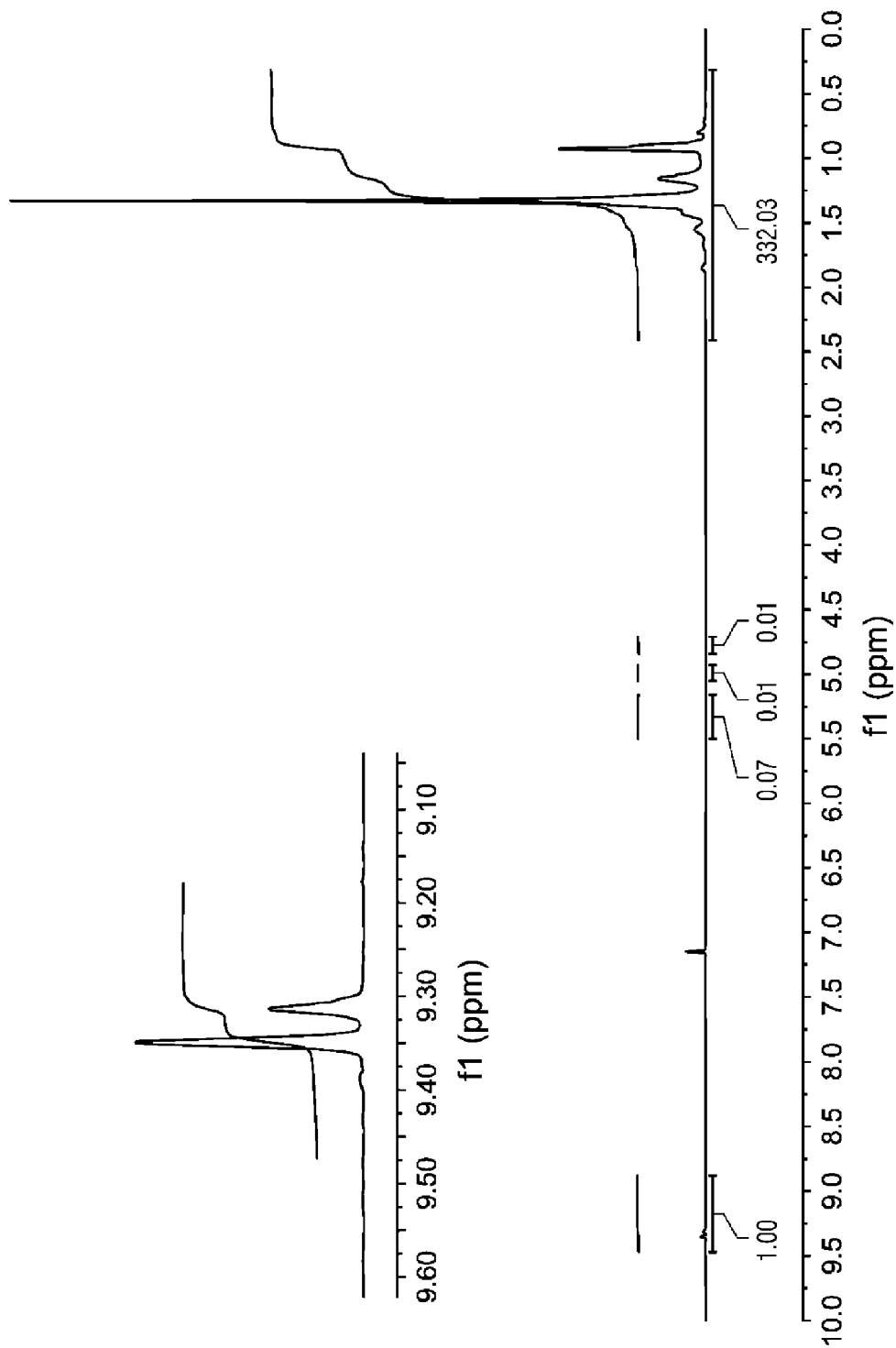


FIG. 8

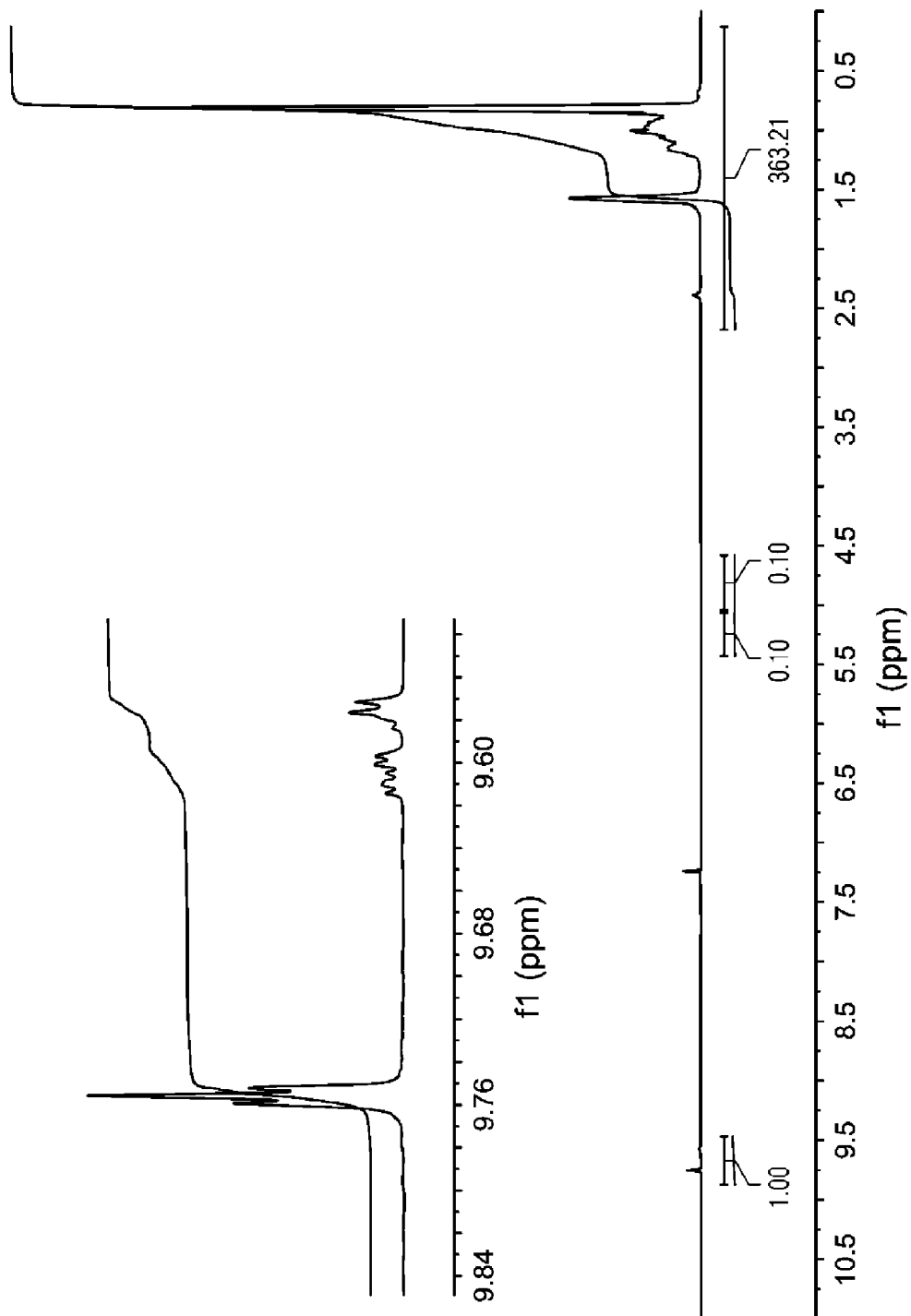


FIG. 9

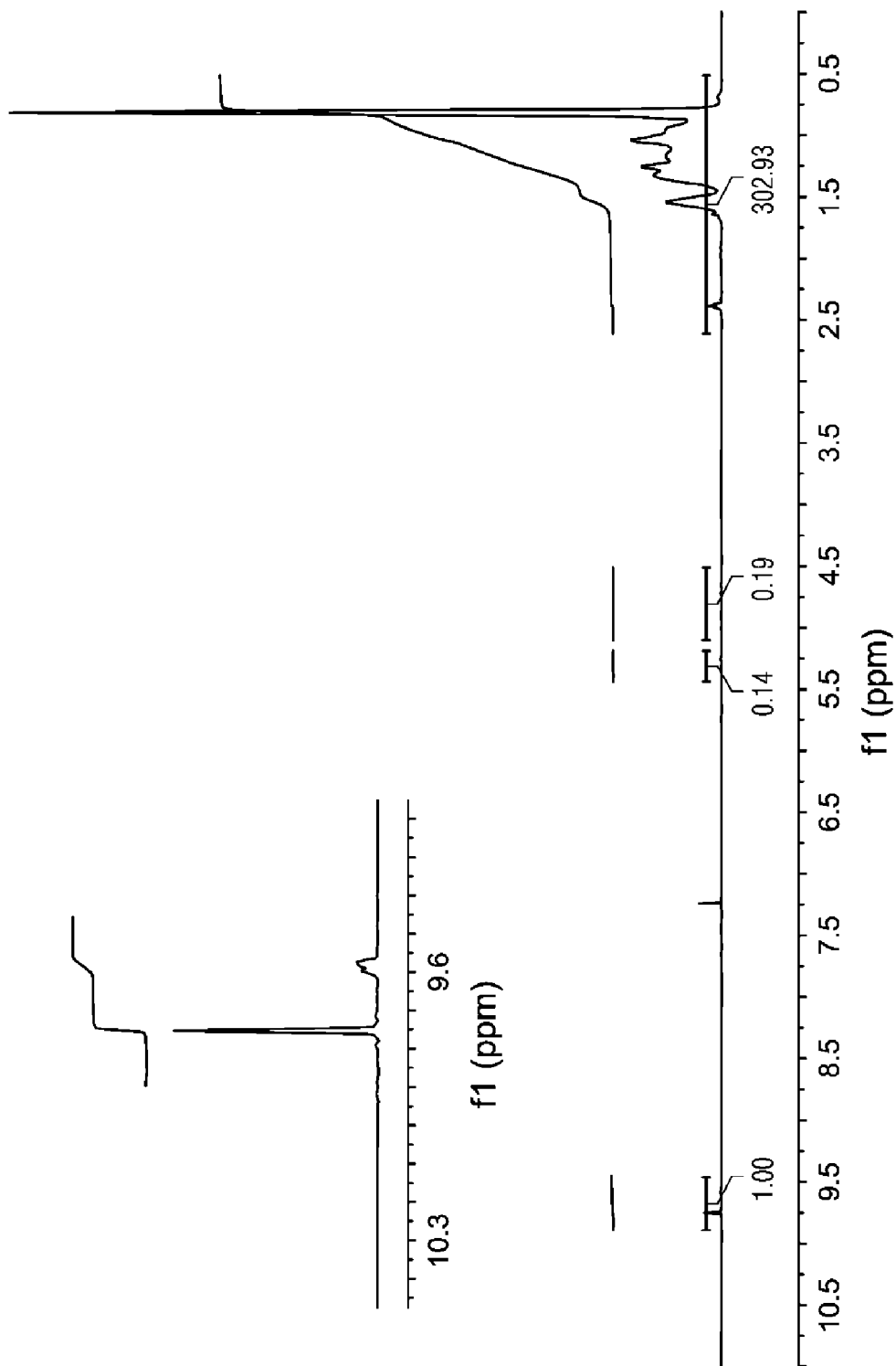


FIG. 10

CATALYTIC HYDROFORMYLATION OF VINYL TERMINATED POLYOLEFINS

CROSS-REFERENCE TO RELATED APPLICATION

This application claims priority to and the benefit of U.S. Provisional Application No. 61/704,639, filed Sep. 24, 2012, the disclosure of which is incorporated herein by reference in its entirety.

FIELD OF THE INVENTION

This invention relates to functionalization of vinyl terminated polyolefins by hydroformylation.

BACKGROUND OF THE INVENTION

Methods for the production of polyolefins with end-functionalized groups are typically multi-step processes that often create unwanted by-products and waste of reactants and energy. For reviews of methods to form end-functionalized polyolefins, see: (a) S. B. Amin and T. J. Marks, *Angewandte Chemie, International Edition*, 2008, 47, pp. 2006-2025; (b) T. C. Chung *Prog. Polym. Sci.* 2002, 27, pp. 39-85; and (c) R. G. Lopez, F. D'Agosto, C. Boisson *Prog. Polym. Sci.* 2007, 32, pp. 419-454. A process with a reduced number of steps, even one step, would be desirable.

U.S. Pat. No. 4,110,377 discloses secondary aliphatic amines alkylated with alpha-olefins, such as ethylene, propylene, hexene, and undecene. Likewise, several literature references disclose hydroaminoalkylation of olefins using various catalysts (see J. Am. Chem. Soc. 2008, 130, pp. 14940-14941; J. Am. Chem. Soc. 2007, 129, pp. 6690-6691; *Angewandte Chemie, International Edition*, 2009, 48, pp. 8361-8365; *Angewandte Chemie, International Edition*, 2009, 48, pp. 4892-4894; *Yuki Gosei Kagaku Kyokaiishi* (2009), 67(8), pp. 843-844; *Angewandte Chemie, International Edition*, (2009), 48(6), pp. 1153-1156; *Tetrahedron Letters* (2003), 44(8), pp. 1679-1683; and *Synthesis* (1980), (4), pp. 305-306). Corey discloses low molecular weight olefins treated with hydrosilanes in the presence of Cp_2MgCl_2 and $n\text{-BuLi}$ to prepare low molecular weight hydrosilylated products.

None of the above references, however, disclose functionalization of polyolefins, particularly polyolefins having Mn 's over 500 g/mol having large amounts of vinyl terminal groups.

U.S. Pat. No. 8,399,725 discloses certain vinyl terminated polymers that are functionalized, optionally, for use in lubricant applications.

U.S. Pat. No. 8,372,930 discloses certain vinyl terminated polymers that are functionalized in U.S. Pat. No. 8,399,725.

U.S. Pat. No. 8,283,419 discloses a process to functionalize propylene homo- or copolymer comprising contacting an alkene metathesis catalyst with a heteroatom containing alkene and a propylene homo- or copolymer having terminal unsaturation.

Additional references of interest include U.S. Pat. Nos. 6,331,656; 5,777,041; P. Mills, Ind. And Eng. Chem. Research, 1990, 29(7) p. 1443 and R. Lazzaroni, J. Mol. Cat. A., 2012, 356, p. 1; WO 94/29018; WO 94/29018; also, U.S. Pat. Nos. 4,320,237; 3,378,590; 3,378,590; 4,049,725; 8,247,618; 8,163,825; 8,143,459; 7,851,221; 7,700,814; 7,586,017; 7,507,868; 7,541,507; 7,422,904; 7,405,329; 7,186,874; 7,148,388; 7,081,554; 7,081,553; 6,982,295; 6,969,736; 6,969,735; 7,405,329; 8,178,730; 7,935,850; EP 1 044 223;

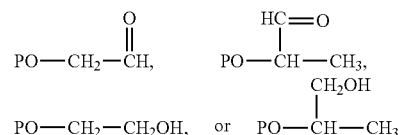
EP 0 804 400; WO 2005/058787, U.S. Pat. Nos. 6,111,027; 7,183,359; 6,100,224; and 5,616,153.

Thus, there is a need to develop a means to provide functionalized polyolefins (particularly end-functionalized) by efficient reactions, particularly reactions with good conversion, preferably under mild reaction conditions with a minimal number of steps, preferably one or two steps. The instant invention's use of hydroformylation to introduce an aldehyde functionality is both a commercially economical and an "atom-economical" route to end-functionalized polyolefins.

End-functionalized polyolefins that feature a chemically reactive or polar end group are of interest for use in a broad range of applications as compatibilizers, tie-layer modifiers, surfactants, adhesives, composites, nanocomposites, pigments, and surface modifiers. They are useful for synthesis of topologically controlled structures such as stars and dendrimers. Herein is described a novel method for their production by the reaction of vinyl-terminated polyolefins with carbon monoxide. This method is useful for a range of vinyl terminated polyolefins, including isotactic polypropylene (iPP), atactic polypropylene (aPP), ethylene propylene copolymer (EP), polyethylene (PE), and, particularly, propylene copolymers with larger alpha-olefin comonomers such as butene, hexene, octene, etc. The vinyl terminated polyolefin useful herein can be linear or branched.

SUMMARY OF THE INVENTION

This invention relates to a polyolefin composition represented by one or more of the following formulae:



wherein the PO is the residual portion of a vinyl terminated macromonomer (VTM) having had a terminal unsaturated carbon of an allylic chain and a vinyl carbon adjacent to the terminal unsaturated carbon; and

wherein the VTM is a vinyl terminated polymer has greater than 30% allyl chain ends with an Mn of greater than, for example 168 (a C_{12} molecule), or greater than 10,000 g/mol.

Hydroformylation is a method for introducing an aldehyde functionality while saturating the double bond. A mixture of the normal- and iso-aldehydes is co-produced.

Vinyl terminated macromonomers (VTMs) with greater than 90% allylic vinyl end groups have been reacted with CO and H_2 (Syngas 1:1.1 molar ratio) using a $\text{Rh}(\text{acac})(\text{CO})_2/\text{PPh}_3$ catalyst. The vinyl chain ends have been converted to aldehydes in high yield. With a higher molar ratio of H_2 to CO of ~2, these same substrates can be converted to alcohols catalytically as well. With this transformation, the functionalized VTMs are rendered useful for a variety of efficient coupling reactions and can be used for applications such as surfactants, coatings, dispersants, compatibilizers (or tie molecules), as well as offering facile pathways to new block polymers.

Catalytic low pressure hydroformylation is thought to work best with allylic vinyl groups and is about three to four times faster than hydroformylation of a vinylidene under the same conditions. On the other hand, allylic vinyl chain ends have been difficult to make, for polyolefins in general, until

recently. With the ability to tailor polyolefin composition and crystallinity, while maintaining >90% allylic vinyl chain ends, it has been found that it is now possible to hydroformylate polyolefin chains under relatively mild conditions and with good yields.

Typically, hydroformylated VTM's are converted to alcohols by known processes, these alcohols being useful for a variety of applications such as intermediates for detergents or plasticizers. The hydroformylated VTM's may be converted to alcohols by a variety of processes, such as the oxo process followed by hydrogenation, or by a modified, single-step oxo process (the modified Shell process), see for instance B. Elvers, et al., Ed., Ullmann's Encyclopedia of Chemical Technology, 5th Ed., Vol. A18, VCH Verlagsgesellschaft mbH, Weinheim, 1991, pp. 321-327. See also Higher Oxo Alcohols, written by Lewis F. Hatch, Enjay Company Inc. 1957, Library of Congress Catalog Card Number 57-13148.

BRIEF DESCRIPTION OF THE FIGURES

FIG. 1 is a FTIR spectrum of hydroformylated product 2 synthesized. Peak assignments: carbonyls 1711 and 1731 cm^{-1} , aldehyde hydrogen 2722 cm^{-1} .

FIG. 2 is a ^{13}C NMR of aPP Aldehyde 2 in C_6D_6 , RT, 250 MHz.

FIG. 3 is a ^{13}C NMR spectrum of C_3C_6 aldehyde 1 in C_6D_6 , RT, 250 MHz.

FIG. 4 is a ^{13}C NMR spectrum of C_2C_3 Aldehyde 3, $\text{C}_2\text{D}_2\text{Cl}_4$, RT, 250 MHz.

FIG. 5 is a ^{13}C NMR of aPP Aldehyde 4 made from 25826-28-2, CDCl_3 , RT, 250 MHz.

FIG. 6 is a ^1H NMR of C_3 aldehyde 2, C_6D_6 , RT, 500 MHz.

FIG. 7 is a ^1H NMR of C_3C_6 aldehyde 1 in C_6D_6 , RT, 500 MHz.

FIG. 8 is a ^1H NMR of C_2C_3 aldehyde 3 in C_6D_6 , RT, 500 MHz.

FIG. 9 is a ^1H NMR of C_3 aldehyde 4 recorded in CDCl_3 , RT, 500 MHz.

FIG. 10 is a ^1H NMR of C_3C_4 Aldehyde 5, recorded in CDCl_3 , RT, 500 MHz.

DEFINITIONS

In the structures depicted throughout this specification and the claims, a solid line indicates a bond and an arrow indicates that the bond may be dative.

As used herein, the new notation for the Periodic Table Groups is used as described in *Chemical and Engineering News*, 63(5), p. 27 (1985).

The term "substituted" means that a hydrogen group has been replaced with a hydrocarbyl group, a heteroatom, or a heteroatom containing group. For example, methyl cyclopentadiene (Cp) is a Cp group substituted with a methyl group and ethyl alcohol is an ethyl group substituted with an —OH group.

The terms "hydrocarbyl radical," "hydrocarbyl," and "hydrocarbyl group" are used interchangeably throughout this document. Likewise, the terms "functional group," "group," and "substituent" are also used interchangeably in this document. For purposes of this disclosure, "hydrocarbyl radical" is defined to be C_1 to C_{20} radicals, that may be linear, branched, or cyclic (aromatic or non-aromatic); and may include substituted hydrocarbyl radicals as defined herein. In an embodiment, a functional group may comprise a hydrocarbyl radical, a substituted hydrocarbyl radical, or a combination thereof.

Substituted hydrocarbyl radicals are radicals in which at least one hydrogen atom has been substituted with a heteroatom or heteroatom containing group, or with atoms from Groups 13, 14, 15, 16, and 17 of the Periodic Table of Elements, or a combination thereof, or with at least one functional group, such as halogen (Cl, Br, I, F), NR^* , OR^* , SeR^* , TeR^* , PR^* , AsR^* , SbR^* , SR^* , BR^* , SiR^* , GeR^* , SnR^* , PbR^* , and the like, or where at least one heteroatom has been inserted within the hydrocarbyl radical, such as halogen (Cl, Br, I, F), O, S, Se, Te, NR^* , PR^* , AsR^* , SbR^* , BR^* , SiR^* , GeR^* , SnR^* , PbR^* , and the like, where R^* is, independently, hydrogen or a hydrocarbyl radical, or any combination thereof.

In an embodiment, the hydrocarbyl radical is independently selected from methyl, ethyl, ethenyl, and isomers of propyl, butyl, pentyl, hexyl, heptyl, octyl, nonyl, decyl, undecyl, dodecyl, tridecyl, tetradecyl, pentadecyl, hexadecyl, heptadecyl, octadecyl, nonadecyl, eicosyl, heneicosyl, docosyl, tricosyl, tetracosyl, pentacosyl, hexacosyl, heptacosyl, octacosyl, nonacosyl, triacontyl, propenyl, butenyl, pentenyl, hexenyl, heptenyl, octenyl, nonenyl, decenyl, undecenyl, dodecenyl, tridecenyl, tetradecenyl, pentadecenyl, hexadecenyl, heptadecenyl, octadecenyl, nonadecenyl, eicosenyl, heneicosenyl, docosenyl, tricosenyl, tetracosenyl, pentacosenyl, hexacosenyl, heptacosenyl, octacosenyl, nonacosenyl, triacontenyl, propynyl, butynyl, pentynyl, hexynyl, heptynyl, octynyl, nonynyl, decynyl, undecynyl, dodecynyl, tridecynyl, tetradecynyl, pentadecynyl, hexadecynyl, heptadecynyl, octadecynyl, nonadecynyl, eicosynyl, heneicosynyl, docosynyl, tricosynyl, tetracosynyl, pentacosynyl, hexacosynyl, heptacosynyl, octacosynyl, nonacosynyl, and triacontynyl. Also included are isomers of saturated, partially unsaturated, and aromatic cyclic structures wherein the radical may additionally be subjected to the types of substitutions described above. Examples include phenyl, methylphenyl, benzyl, methylbenzyl, naphthyl, cyclohexyl, cyclohexenyl, methylcyclohexyl, and the like. For this disclosure, when a radical is listed, it indicates that radical type and all other radicals formed when that radical type is subjected to the substitutions defined above. Alkyl, alkenyl, and alkynyl radicals listed include all isomers including, where appropriate, cyclic isomers, for example, butyl includes n-butyl, 2-methylpropyl, 1-methylpropyl, tert-butyl, and cyclobutyl (and analogous substituted cyclopropyls); pentyl includes n-pentyl, cyclopentyl, 1-methylbutyl, 2-methylbutyl, 3-methylbutyl, 1-ethylpropyl, and neopentyl (analogous substituted cyclobutyls and cyclopropyls); and butenyl includes E and Z forms of 1-butenyl, 2-butenyl, 3-butenyl, 1-methyl-1-propenyl, 1-methyl-2-propenyl, 2-methyl-1-propenyl, and 2-methyl-2-propenyl (cyclobutenyls and cyclopropenyls). Cyclic compounds having substitutions include all isomer forms, for example, methylphenyl would include ortho-methylphenyl, meta-methylphenyl, and para-methylphenyl; dimethylphenyl would include 2,3-dimethylphenyl, 2,4-dimethylphenyl, 2,5-dimethylphenyl, 2,6-diphenylmethyl, 3,4-dimethylphenyl, and 3,5-dimethylphenyl.

An "olefin," alternatively referred to as "alkene," is a linear, branched, or cyclic compound of carbon and hydrogen having at least one double bond. For purposes of this specification and the claims appended thereto, when a polymer or copolymer is referred to as comprising an olefin, including, but not limited to, ethylene, propylene, and butene, the olefin present in such polymer or copolymer is the polymerized form of the olefin. For example, when a copolymer is said to have an "ethylene" content of 35 wt % to 55 wt %, it is understood that the mer unit in the copolymer is derived from ethylene in the polymerization reaction and said derived units

are present at 35 wt % to 55 wt %, based upon the weight of the copolymer. A "polymer" has two or more of the same or different mer units. A "homopolymer" is a polymer having mer units that are the same. A "copolymer" is a polymer having two or more mer units that are different from each other. A "terpolymer" is a polymer having three mer units that are different from each other. "Different" as used to refer to mer units indicates that the mer units differ from each other by at least one atom or are different isomerically. Accordingly, the definition of copolymer, as used herein, includes terpolymers and the like. An oligomer is a polymer having a low molecular weight. In some embodiments, an oligomer has an Mn of 21,000 g/mol or less (e.g., 2,500 g/mol or less); in other embodiments, an oligomer has a low number of mer units (such as 75 mer units or less).

An "alpha-olefin" is an olefin having a double bond at the alpha (or 1-) position. A "linear alpha-olefin" or "LAO" is an olefin with a double bond at the alpha position and a linear hydrocarbon chain. A "polyalphaolefin" or "PAO" is a polymer having two or more alpha-olefin units. For the purposes of this disclosure, the term " α -olefin" includes C_2 - C_{20} olefins. Non-limiting examples of α -olefins include ethylene, propylene, 1-butene, 1-pentene, 1-hexene, 1-heptene, 1-octene, 1-nonene, 1-decene, 1-undecene, 1-dodecene, 1-tridecene, 1-tetradecene, 1-pentadecene, 1-hexadecene, 1-heptadecene, 1-octadecene, 1-nonadecene, 1-eicosene, 1-heneicosene, 1-docosene, 1-tricosene, 1-tetracosene, 1-pentacosene, 1-hexacosene, 1-heptacosene, 1-octacosene, 1-nonacosene, 1-triacontene, 4-methyl-1-pentene, 3-methyl-1-pentene, 5-methyl-1-nonene, 3,5,5-trimethyl-1-hexene, vinylcyclohexane, and vinylnorbornane. Non-limiting examples of cyclic olefins and diolefins include cyclopropene, cyclobutene, cyclopentene, cyclohexene, cycloheptene, cyclooctene, cyclononene, cyclodecene, norbornene, 4-methylnorbornene, 2-methylcyclopentene, 4-methylcyclopentene, vinylcyclohexane, norbornadiene, dicyclopentadiene, 5-ethylidene-2-norbornene, vinylcyclohexene, 5-vinyl-2-norbornene, 1,3-divinylcyclopentane, 1,2-divinylcyclohexane, 1,3-divinylcyclohexane, 1,4-divinylcyclohexane, 1,5-divinylcyclooctane, 1-allyl-4-vinylcyclohexane, 1,4-diallylcyclohexane, 1-allyl-5-vinylcyclooctane, and 1,5-diallylcyclooctane.

For purposes herein, a polymer or polymeric chain comprises a concatenation of carbon atoms bonded to each other in a linear or a branched chain, which is referred to herein as the backbone of the polymer (e.g., polyethylene). The polymeric chain may further comprise various pendent groups attached to the polymer backbone which were present on the monomers from which the polymer was produced. These pendent groups are not to be confused with branching of the polymer backbone, the difference between pendent side chains and both short and long chain branching being readily understood by one of skill in the art.

The terms "catalyst" and "catalyst compound" are defined to mean a compound capable of initiating catalysis. In the description herein, the catalyst may be described as a catalyst precursor, a pre-catalyst compound, or a transition metal compound (for example, a metallocene compound), and these terms are used interchangeably. A catalyst compound may be used by itself to initiate catalysis or may be used in combination with an activator to initiate catalysis. When the catalyst compound is combined with an activator to initiate catalysis, the catalyst compound is often referred to as a pre-catalyst or catalyst precursor. A "catalyst system" is a combination of at least one catalyst compound, an optional activator, an optional co-activator, and an optional support material, where the system can polymerize monomers to polymer. For the

purposes of this invention and the claims thereto, when catalyst systems are described as comprising neutral stable forms of the components, it is well understood by one of ordinary skill in the art, that the ionic form of the component is the form that reacts with the monomers to produce polymers.

An "anionic ligand" is a negatively charged ligand which donates one or more pairs of electrons to a metal ion. A "neutral donor ligand" is a neutrally charged ligand which donates one or more pairs of electrons to a metal ion.

A "scavenger" is a compound that is typically added to facilitate polymerization by scavenging impurities. Some scavengers may also act as activators and may be referred to as co-activators. A co-activator, that is not a scavenger, may also be used in conjunction with an activator in order to form an active catalyst. In some embodiments, a co-activator can be pre-mixed with the catalyst compound to form an alkylated catalyst compound, also referred to as an alkylated invention compound.

A propylene polymer is a polymer having at least 50 mol % of propylene. As used herein, Mn is number average molecular weight as determined by proton nuclear magnetic resonance spectroscopy (1H NMR) where, unless otherwise stated, the data is collected at 120° C. in a 5 mm probe using a spectrometer with a 1H frequency of at least 400 MHz. Data is recorded using a maximum pulse width of 45°, 8 seconds between pulses, and signal averaging 120 transients. Unless stated otherwise, Mw is weight average molecular weight as determined by gel permeation chromatography (GPC). Mz is z average molecular weight as determined by GPC as described in the VINYL TERMINATED MACROMONOMERS section below, wt % is weight percent, and mol % is mole percent. Molecular weight distribution (MWD) is defined to be Mw (GPC) divided by Mn (GPC). Unless otherwise noted, all molecular weight units, e.g., Mw, Mn, Mz, are g/mol.

The following abbreviations may be used through this specification: Me is methyl, Ph is phenyl, Et is ethyl, Pr is propyl, iPr is isopropyl, n-Pr is normal propyl, Bu is butyl, iBu is isobutyl, tBu is tertiary butyl, p-tBu is para-tertiary butyl, nBu is normal butyl, TMS is trimethylsilyl, TIBAL is triisobutylaluminum, TNOAL is triisobutyl n-octylaluminum, MAO is methylalumoxane, pMe is para-methyl, Ar* is 2,6-diisopropylaryl, Bz is benzyl, THF is tetrahydrofuran, and "tol" is toluene, and acac is acetylacetonate.

DETAILED DESCRIPTION OF THE INVENTION

Amorphous polyolefin backbones with polyamine (PAM) functionalization, such as the reaction products between polyisobutylene succinic anhydride (PIB-SA) and polyamine (PAM), commonly known as PIB-SA-PAM, can serve as dispersants, corrosion inhibitors, detergents in lubricating oil, fuel and oil (gas) transportation pipeline applications, etc. The present invention provides vinyl-terminated macromonomers (VTM) that have been hydroformylated to the aldehyde-functionalized macromonomers. These materials are expected to exhibit performance advantages over commercial PIB-SA-PAM containing materials.

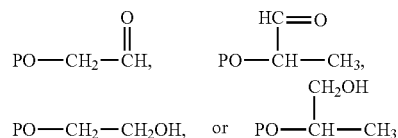
Hydroformylation of simple low-molecular weight olefins is a well-known method for introducing an aldehyde functionality while saturating the double bond. Usually a mixture of the normal- and iso-aldehydes is co-produced. Subsequent conversion of the aldehyde group to other functionalities by either oxidation or reduction methods are also known.

The present invention discloses a method of functionalizing high vinyl content terminated macromonomers by hydroformylation to produce aldehyde containing polyolefins. The

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functionalized polyolefin chain can vary greatly in molecular weights, polydispersity, tacticity, co-monomer composition, and incorporated functionality.

This invention relates to a polyolefin composition represented by one or more of the following formulae:



wherein the PO is the residual portion of a vinyl terminated macromonomer (VTM) having had a terminal unsaturated carbon of an allylic chain and a vinyl carbon adjacent to the terminal unsaturated carbon; and

wherein the VTM is a vinyl terminated polymer having at least 5% allyl chain ends (preferably greater than 30% allyl chain ends with an Mn of 16 g/mol or more, alternately greater than 10,000 g/mol).

In certain aspects, the VTM is one or more of:

- (i) a vinyl terminated polymer having at least 5% allyl chain ends (preferably 15%, 20%, 30%, 40%, 50%, 60%, 70%, 80%, 90%, 95%, 98%, or 99%);
- (ii) a vinyl terminated polymer having an Mn of at least 160 g/mol, preferably at least 200 g/mol (measured by ^1H NMR) comprising of one or more C_4 to C_{40} higher olefin derived units, where the higher olefin polymer comprises substantially no propylene derived units, and wherein the higher olefin polymer has at least 5% allyl chain ends;
- (iii) a copolymer having an Mn of 300 g/mol or more (measured by ^1H NMR) comprising (a) from about 20 mol % to about 99.9 mol % of at least one C_5 to C_{40} higher olefin, and (b) from about 0.1 mol % to about 80 mol % of propylene, wherein the higher olefin copolymer has at least 40% allyl chain ends;
- (iv) a copolymer having an Mn of 300 g/mol or more (measured by ^1H NMR), and comprises (a) from about 80 mol % to about 99.9 mol % of at least one C_4 olefin, (b) from about 0.1 mol % to about 20 mol % of propylene; and wherein the vinyl terminated macromonomer has at least 40% allyl chain ends relative to total unsaturation;
- (v) a co-oligomer having an Mn of 300 g/mol to 30,000 g/mol (measured by ^1H NMR) comprising 10 mol % to 90 mol % propylene and 10 mol % to 90 mol % of ethylene, wherein the oligomer has at least X % allyl chain ends (relative to total unsaturations), where: 1) $X = (-0.94 * (\text{mol \% ethylene incorporated}) + 100)$, when 10 mol % to 60 mol % ethylene is present in the co-oligomer, 2) $X = 45$, when greater than 60 mol % and less than 70 mol % ethylene is present in the co-oligomer, and 3) $X = (1.83 * (\text{mol \% ethylene incorporated}) - 83)$, when 70 mol % to 90 mol % ethylene is present in the co-oligomer;
- (vi) a propylene oligomer, comprising more than 90 mol % propylene and less than 10 mol % ethylene wherein the oligomer has: at least 93% allyl chain ends, a number average molecular weight (Mn) of about 500 g/mol to about 20,000 g/mol, an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.35:1.0, less than 100 ppm aluminum, and/or less than 250 regio defects per 10,000 monomer units;
- (vii) a propylene oligomer, comprising: at least 50 mol % propylene and from 10 mol % to 50 mol % ethylene, wherein the oligomer has: at least 90% allyl chain ends, an Mn of about 150 g/mol to about 20,000 g/mol, preferably

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10,000 g/mol, and an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.2:1.0, wherein monomers having four or more carbon atoms are present at from 0 mol % to 3 mol %;

- (viii) a propylene oligomer, comprising: at least 50 mol % propylene, from 0.1 mol % to 45 mol % ethylene, and from 0.1 mol % to 5 mol % C_4 to C_{12} olefin, wherein the oligomer has: at least 90% allyl chain ends, an Mn of about 150 g/mol to about 10,000 g/mol, and an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.35:1.0;
- (ix) a propylene oligomer, comprising: at least 50 mol % propylene, from 0.1 mol % to 45 mol % ethylene, and from 0.1 mol % to 5 mol % diene, wherein the oligomer has: at least 90% allyl chain ends, an Mn of about 150 g/mol to about 10,000 g/mol, and an isobutyl chain end to allylic vinyl group ratio of 0.7:1 to 1.35:1.0;
- (x) a homo-oligomer, comprising propylene, wherein the oligomer has: at least 93% allyl chain ends, an Mn of about 500 g/mol to about 70,000 g/mol, alternately to about 20,000 g/mol, an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.2:1.0, and less than 1400 ppm aluminum;
- (xi) vinyl terminated polyethylene having: (a) at least 60% allyl chain ends, (b) a molecular weight distribution of less than or equal to 4.0, (c) a $g'(\text{vis})$ of greater than 0.95, and (d) an Mn (^1H NMR) of at least 20,000 g/mol; and
- (xii) vinyl terminated polyethylene having: (a) at least 50% allyl chain ends, (b) a molecular weight distribution of less than or equal to 4.0, (c) a $g'(\text{vis})$ of 0.95 or less, (d) an Mn (^1H NMR) of at least 7,000 g/mol, and (e) a Mn (GPC)/Mn (^1H NMR) in the range of from about 0.8 to about 1.2.

Vinyl Terminated Macromonomers

A "vinyl terminated macromonomer," (also referred to as a "vinyl terminated polyolefin") as used herein, refers to one or more of:

- (i) a vinyl terminated polymer having at least 5% allyl chain ends (preferably 15%, 20%, 30%, 40%, 50%, 60%, 70%, 80%, 90%, 95%, 98%, or 99%);
- (ii) a vinyl terminated polymer having an Mn of at least 160 g/mol, preferably at least 200 g/mol (measured by ^1H NMR) comprising of one or more C_4 to C_{40} higher olefin derived units, where the higher olefin polymer comprises substantially no propylene derived units, and wherein the higher olefin polymer has at least 5% allyl chain ends;
- (iii) a copolymer having an Mn of 300 g/mol or more (measured by ^1H NMR) comprising (a) from about 20 mol % to about 99.9 mol % of at least one C_5 to C_{40} higher olefin, and (b) from about 0.1 mol % to about 80 mol % of propylene, wherein the higher olefin copolymer has at least 40% allyl chain ends;
- (iv) a copolymer having an Mn of 300 g/mol or more (measured by ^1H NMR), and comprises (a) from about 80 mol % to about 99.9 mol % of at least one C_4 olefin, (b) from about 0.1 mol % to about 20 mol % of propylene, and wherein the vinyl terminated macromonomer has at least 40% allyl chain ends relative to total unsaturation;
- (v) a co-oligomer having an Mn of 300 g/mol to 30,000 g/mol (measured by ^1H NMR) comprising 10 mol % to 90 mol % propylene and 10 mol % to 90 mol % of ethylene, wherein the oligomer has at least X % allyl chain ends (relative to total unsaturations), where: 1) $X = (-0.94 * (\text{mol \% ethylene incorporated}) + 100)$, when 10 mol % to 60 mol % ethylene is present in the co-oligomer, 2) $X = 45$, when greater than 60 mol % and less than 70 mol % ethylene is present in the co-oligomer, and 3) $X = (1.83 * (\text{mol \% ethylene incorporated}) - 83)$, when 70 mol % to 90 mol % ethylene is present in the co-oligomer;

- (vi) a propylene oligomer, comprising more than 90 mol % propylene and less than 10 mol % ethylene wherein the oligomer has: at least 93% allyl chain ends, a number average molecular weight (Mn) of about 500 g/mol to about 20,000 g/mol, an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.35:1.0, less than 100 ppm aluminum, and/or less than 250 regio defects per 10,000 monomer units;
- (vii) a propylene oligomer, comprising: at least 50 mol % propylene and from 10 mol % to 50 mol % ethylene, wherein the oligomer has: at least 90% allyl chain ends, an Mn of about 150 g/mol to about 20,000 g/mol, preferably 10,000 g/mol, and an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.2:1.0, wherein monomers having four or more carbon atoms are present at from 0 mol % to 3 mol %;
- (viii) a propylene oligomer, comprising: at least 50 mol % propylene, from 0.1 mol % to 45 mol % ethylene, and from 0.1 mol % to 5 mol % C₄ to C₁₂ olefin, wherein the oligomer has: at least 90% allyl chain ends, an Mn of about 150 g/mol to about 10,000 g/mol, and an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.35:1.0;
- (ix) a propylene oligomer, comprising: at least 50 mol % propylene, from 0.1 mol % to 45 mol % ethylene, and from 0.1 mol % to 5 mol % diene, wherein the oligomer has: at least 90% allyl chain ends, an Mn of about 150 g/mol to about 10,000 g/mol, and an isobutyl chain end to allylic vinyl group ratio of 0.7:1 to 1.35:1.0;
- (x) a homo-oligomer, comprising propylene, wherein the oligomer has: at least 93% allyl chain ends, an Mn of about 500 g/mol to about 70,000 g/mol, alternately to about 20,000 g/mol, an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.2:1.0, and less than 1400 ppm aluminum;
- (xi) vinyl terminated polyethylene having: (a) at least 60% allyl chain ends, (b) a molecular weight distribution of less than or equal to 4.0, (c) a $g'_{(v_{ts})}$ of greater than 0.95, and (d) an Mn (¹H NMR) of at least 20,000 g/mol; and
- (xii) vinyl terminated polyethylene having: (a) at least 50% allyl chain ends, (b) a molecular weight distribution of less than or equal to 4.0, (c) a $g'_{(v_{ts})}$ of 0.95 or less, (d) an Mn (¹H NMR) of at least 7,000 g/mol, and (e) a Mn (GPC)/Mn (¹H NMR) in the range of from about 0.8 to about 1.2.

It is understood by those of ordinary skill in the art that when the VTM's, as described here, are reacted with another material the "vinyl" (e.g. the allyl chain end) is involved in the reaction and has been transformed. Thus, the language used herein describing that a fragment of the final product (typically referred to as PO in the formulae herein) is the residual portion of a vinyl terminated macromonomer (VTM) having had a terminal unsaturated carbon of an allylic chain and a vinyl carbon adjacent to the terminal unsaturated carbon, is meant to refer to the fact that the VTM has been incorporated in the product. Similarly stating that a product or material comprises a VTM means that the reacted form of the VTM is present, unless the context clearly indicates otherwise (such as a mixture of ingredients that do not have a catalytic agent present.)

In some embodiments, the vinyl terminated macromonomer has an Mn of at least 200 g/mol, (e.g., 200 g/mol to 100,000 g/mol, e.g., 200 g/mol to 75,000 g/mol, e.g., 200 g/mol to 60,000 g/mol, e.g., 300 g/mol to 60,000 g/mol, e.g., 750 g/mol to 30,000 g/mol) (measured by ¹H NMR) and comprises one or more (e.g., two or more, three or more, four or more, and the like) C₄ to C₄₀ (e.g., C₄ to C₃₀, C₄ to C₂₀, or C₄ to C₁₂, e.g., butene, pentene, hexene, heptene, octene, nonene, decene, undecene, dodecene, norbornene, norbornadiene, dicyclopentadiene, cyclopentene, cycloheptene,

cyclooctene, cyclooctadiene, cyclododecene, 7-oxanorbornene, 7-oxanorbornadiene, substituted derivatives thereof, and isomers thereof) olefin derived units, where the vinyl terminated macromonomer comprises substantially no propylene derived units (e.g., less than 0.1 wt % propylene, e.g., 0 wt %); and wherein the vinyl terminated macromonomer has at least 5% (at least 10%, at least 15%, at least 20%, at least 30%, at least 40%, at least 50%, at least 60%, at least 70%; at least 80%, at least 90%, or at least 95%) allyl chain ends (relative to total unsaturation); and, optionally, an allyl chain end to vinylidene chain end ratio of 1:1 or greater (e.g., greater than 2:1, greater than 2.5:1, greater than 3:1, greater than 5:1, or greater than 10:1); and even further, optionally, e.g., substantially no isobutyl chain ends (e.g., less than 0.1 wt % isobutyl chain ends). In some embodiments, the vinyl terminated macromonomers may also comprise ethylene derived units, e.g., at least 5 mol % ethylene (e.g., at least 15 mol % ethylene, e.g., at least 25 mol % ethylene, e.g., at least 35 mol % ethylene, e.g., at least 45 mol % ethylene, e.g., at least 60 mol % ethylene, e.g., at least 75 mol % ethylene, or e.g., at least 90 mol % ethylene). Such vinyl terminated macromonomers are further described in U.S. Pat. No. 8,426,659, which is hereby incorporated by reference.

In some embodiments, the vinyl terminated macromonomers may have an Mn (measured by ¹H NMR) of greater than 200 g/mol (e.g., 300 g/mol to 60,000 g/mol, 400 g/mol to 50,000 g/mol, 500 g/mol to 35,000 g/mol, 300 g/mol to 15,000 g/mol, 400 g/mol to 12,000 g/mol, or 750 g/mol to 10,000 g/mol), and comprise:

- (a) from about 20 mol % to 99.9 mol % (e.g., from about 25 mol % to about 90 mol %, from about 30 mol % to about 85 mol %, from about 35 mol % to about 80 mol %, from about 40 mol % to about 75 mol %, or from about 50 mol % to about 95 mol %) of at least one C₅ to C₄₀ (e.g., C₆ to C₂₀) higher olefin;
- (b) from about 0.1 mol % to 80 mol % (e.g., from about 5 mol % to 70 mol %, from about 10 mol % to about 65 mol %, from about 15 mol % to about 55 mol %, from about 25 mol % to about 50 mol %, or from about 30 mol % to about 80 mol %) of propylene; and

wherein the vinyl terminated macromonomer has at least 40% allyl chain ends (e.g., at least 50% allyl chain ends, at least 60% allyl chain ends, at least 70% allyl chain ends, at least 80% allyl chain ends, at least 90% allyl chain ends, or at least 95% allyl chain ends) relative to total unsaturation; and, optionally, an isobutyl chain end to allyl chain end ratio of less than 0.70:1, less than 0.65:1, less than 0.60:1, less than 0.50:1, or less than 0.25:1; and further, optionally, an allyl chain end to vinylidene chain end ratio of greater than 2:1 (e.g., greater than 2.5:1, greater than 3:1, greater than 5:1, or greater than 10:1); and even further, optionally, an allyl chain end to vinylene ratio is greater than 1:1 (e.g., greater than 2:1 or greater than 5:1). Such macromonomers are further described in U.S. Pat. No. 8,399,724, hereby incorporated by reference.

In another embodiment, the vinyl terminated macromonomer has an Mn of 300 g/mol or more (measured by ¹H NMR, e.g., 300 g/mol to 60,000 g/mol, 400 g/mol to 50,000 g/mol, 500 g/mol to 35,000 g/mol, 300 g/mol to 15,000 g/mol, 400 g/mol to 12,000 g/mol, or 750 g/mol to 10,000 g/mol), and comprises:

- (a) from about 80 mol % to about 99.9 mol % of at least one C₄ olefin, e.g., about 85 mol % to about 99.9 mol %, about 90 mol % to about 99.9 mol %;
- (b) from about 0.1 mol % to about 20 mol % of propylene, e.g., about 0.1 mol % to about 15 mol %, e.g., about 0.1 mol % to about 10 mol %; and

wherein the vinyl terminated macromonomer has at least 40% allyl chain ends (e.g., at least 50% allyl chain ends, at least 60% allyl chain ends, at least 70% allyl chain ends, or at least 80% allyl chain ends, at least 90% allyl chain ends, at least 95% allyl chain ends) relative to total unsaturation, and, in some embodiments, an isobutyl chain end to allyl chain end ratio of less than 0.70:1, less than 0.65:1, less than 0.60:1, less than 0.50:1, or less than 0.25:1, and, in further embodiments, an allyl chain end to vinylidene group ratio of more than 2:1, more than 2.5:1, more than 3:1, more than 5:1, or more than 10:1. Such macromonomers are also further described in U.S. Pat. No. 8,399,724, which is hereby incorporated by reference.

In other embodiments, the vinyl terminated macromonomer is a propylene co-oligomer having an Mn of 300 g/mol to 30,000 g/mol as measured by ^1H NMR (e.g., 400 g/mol to 20,000 g/mol, e.g., 500 g/mol to 15,000 g/mol, e.g., 600 g/mol to 12,000 g/mol, e.g., 800 g/mol to 10,000 g/mol, e.g., 900 g/mol to 8,000 g/mol, e.g., 900 g/mol to 7,000 g/mol), comprising 10 mol % to 90 mol % propylene (e.g., 15 mol % to 85 mol %, e.g., 20 mol % to 80 mol %, e.g., 30 mol % to 75 mol %, e.g., 50 mol % to 90 mol %) and 10 mol % to 90 mol % (e.g., 85 mol % to 15 mol %, e.g., 20 mol % to 80 mol %, e.g., 25 mol % to 70 mol %, e.g., 10 mol % to 50 mol %) of one or more alpha-olefin comonomers (e.g., ethylene, butene, hexene, or octene, e.g., ethylene), wherein the oligomer has at least X % allyl chain ends (relative to total unsaturations), where: 1) $X = (-0.94 (\text{mol \% ethylene incorporated}) + 100)$ {alternately $1.20 (-0.94 (\text{mol \% ethylene incorporated}) + 100)$, alternately $1.50 (-0.94 (\text{mol \% ethylene incorporated}) + 100)$ }, when 10 mol % to 60 mol % ethylene is present in the co-oligomer; 2) $X = 45$ (alternately 50, alternately 60), when greater than 60 mol % and less than 70 mol % ethylene is present in the co-oligomer; and 3) $X = (1.83 * (\text{mol \% ethylene incorporated}) - 83)$, {alternately $1.20 [1.83 * (\text{mol \% ethylene incorporated}) - 83]$, alternately $1.50 [1.83 * (\text{mol \% ethylene incorporated}) - 83]$ }, when 70 mol % to 90 mol % ethylene is present in the co-oligomer. Such macromonomers are further described in U.S. Pat. No. 8,372,930, which is hereby incorporated by reference.

In other embodiments, the vinyl terminated macromonomer is a propylene oligomer, comprising more than 90 mol % propylene (e.g., 95 mol % to 99 mol %, e.g., 98 mol % to 9 mol %) and less than 10 mol % ethylene (e.g., 1 mol % to 4 mol %, e.g., 1 mol % to 2 mol %), wherein the oligomer has: at least 93% allyl chain ends (e.g., at least 95%, e.g., at least 97%, e.g., at least 98%); a number average molecular weight (Mn) of about 400 g/mol to about 30,000 g/mol, as measured by ^1H NMR (e.g., 500 g/mol to 20,000 g/mol, e.g., 600 g/mol to 15,000 g/mol, e.g., 700 g/mol to 10,000 g/mol, e.g., 800 g/mol to 9,000 g/mol, e.g., 900 g/mol to 8,000 g/mol, e.g., 1,000 g/mol to 6,000 g/mol); an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.35:1.0, and less than 1400 ppm aluminum (e.g., less than 1200 ppm, e.g., less than 1000 ppm, e.g., less than 500 ppm, e.g., less than 100 ppm). Such macromonomers are further described in U.S. Pat. No. 8,372,930.

In other embodiments, the vinyl terminated macromonomer is a propylene oligomer, comprising: at least 50 mol % (e.g., 60 mol % to 90 mol %, e.g., 70 mol % to 90 mol %) propylene and from 10 mol % to 50 mol % (e.g., 10 mol % to 40 mol %, e.g., 10 mol % to 30 mol %) ethylene, wherein the oligomer has: at least 90% allyl chain ends (e.g., at least 91%, e.g., at least 93%, e.g., at least 95%, e.g., at least 98%); an Mn of about 150 g/mol to about 20,000 g/mol, as measured by ^1H NMR (e.g., 200 g/mol to 15,000 g/mol, e.g., 250 g/mol to 15,000 g/mol, e.g., 300 g/mol to 10,000 g/mol, e.g., 400 g/mol to 9,500 g/mol, e.g., 500 g/mol to 9,000 g/mol, e.g., 750 g/mol

to 9,000 g/mol); and an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.3:1.0, wherein monomers having four or more carbon atoms are present at from 0 mol % to 3 mol % (e.g., at less than 1 mol %, e.g., at less than 0.5 mol %, e.g., at 0 mol %). Such macromonomers are further described in U.S. Pat. No. 8,372,930.

In other embodiments, the vinyl terminated macromonomer is a propylene oligomer, comprising: at least 50 mol % (e.g., at least 60 mol %, e.g., 70 mol % to 99.5 mol %, e.g., 80 mol % to 99 mol %, e.g., 90 mol % to 98.5 mol %) propylene, from 0.1 mol % to 45 mol % (e.g., at least 35 mol %, e.g., 0.5 mol % to 30 mol %, e.g., 1 mol % to 20 mol %, e.g., 1.5 mol % to 10 mol %) ethylene, and from 0.1 mol % to 5 mol % (e.g., 0.5 mol % to 3 mol %, e.g., 0.5 mol % to 1 mol %) C_4 to C_{12} olefin (such as butene, hexene, or octene, e.g., butene), wherein the oligomer has: at least 90% allyl chain ends (e.g., at least 91%, e.g., at least 93%, e.g., at least 95%, e.g., at least 98%); a number average molecular weight (Mn) of about 150 g/mol to about 15,000 g/mol, as measured by ^1H NMR (e.g., 200 g/mol to 12,000 g/mol, e.g., 250 g/mol to 10,000 g/mol, e.g., 300 g/mol to 10,000 g/mol, e.g., 400 g/mol to 9,500 g/mol, e.g., 500 g/mol to 9,000 g/mol, e.g., 750 g/mol to 9,000 g/mol); and an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.35:1.0. Such macromonomers are further described in U.S. Pat. No. 8,372,930.

In other embodiments, the vinyl terminated macromonomer is a propylene oligomer, comprising: at least 50 mol % (e.g., at least 60 mol %, e.g., 70 mol % to 99.5 mol %, e.g., 80 mol % to 99 mol %, e.g., 90 mol % to 98.5 mol %) propylene, from 0.1 mol % to 45 mol % (e.g., at least 35 mol %, e.g., 0.5 mol % to 30 mol %, e.g., 1 mol % to 20 mol %, e.g., 1.5 mol % to 10 mol %) ethylene, and from 0.1 mol % to 5 mol % (e.g., 0.5 mol % to 3 mol %, e.g., 0.5 mol % to 1 mol %) diene (such as C_4 to C_{12} alpha-omega dienes (such as butadiene, hexadiene, octadiene, norbornene, ethylidene norbornene, vinylnorbornene, norbornadiene, and dicyclopentadiene), wherein the oligomer has at least 90% allyl chain ends (e.g., at least 91%, e.g., at least 93%, e.g., at least 95%, e.g., at least 98%); a number average molecular weight (Mn) of about 150 g/mol to about 20,000 g/mol, as measured by ^1H NMR (e.g., 200 g/mol to 15,000 g/mol, e.g., 250 g/mol to 12,000 g/mol, e.g., 300 g/mol to 10,000 g/mol, e.g., 400 g/mol to 9,500 g/mol, e.g., 500 g/mol to 9,000 g/mol, e.g., 750 g/mol to 9,000 g/mol); and an isobutyl chain end to allylic vinyl group ratio of 0.7:1 to 1.35:1.0. Such macromonomers are further described in U.S. Pat. No. 8,372,930.

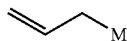
In other embodiments, the vinyl terminated macromonomer is a propylene homo-oligomer, comprising propylene and less than 0.5 wt % comonomer, e.g., 0 wt % comonomer, wherein the oligomer has:

- i) at least 93% allyl chain ends (e.g., at least 95%, e.g., at least 96%, e.g., at least 97%, e.g., at least 98%, e.g., at least 99%);
- ii) a number average molecular weight (Mn) of about 500 g/mol to about 20,000 g/mol, as measured by ^1H NMR (e.g., 500 g/mol to 15,000 g/mol, e.g., 700 g/mol to 10,000 g/mol, e.g., 800 g/mol to 8,000 g/mol, e.g., 900 g/mol to 7,000 g/mol, e.g., 1,000 g/mol to 6,000 g/mol, e.g., 1,000 g/mol to 5,000 g/mol);
- iii) an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.3:1.0; and
- iv) less than 1400 ppm aluminum, (e.g., less than 1200 ppm, e.g., less than 1000 ppm, e.g., less than 500 ppm, e.g., less than 100 ppm). Such macromonomers are also further described in U.S. Pat. No. 8,372,930.

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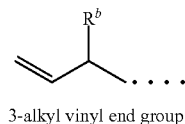
- The vinyl terminated macromonomers may be homopolymers, copolymers, terpolymers, and so on. Any vinyl terminated macromonomers described herein has one or more of:
- (i) an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.3:1.0;
 - (ii) an allyl chain end to vinylidene chain end ratio of greater than 2:1 (e.g., greater than 2.5:1, greater than 3:1, greater than 5:1, or greater than 10:1);
 - (iii) an allyl chain end to vinylene ratio is greater than 1:1 (e.g., greater than 2:1 or greater than 5:1); and
 - (iv) at least 5% allyl chain ends (preferably 15%, 20%, 30%, 40%, 50%, 60%, 70%, 80%, 90%, 95%, 98%, or 99%).

Vinyl terminated macromonomers generally have a saturated chain end (or terminus) and/or an unsaturated chain end (or terminus). The unsaturated chain end of the vinyl terminated macromonomer comprises an "allyl chain end" or a "3-alkyl" chain end. An allyl chain end is represented by $\text{CH}_2\text{CH}=\text{CH}_2$, as shown in the formula:



where M represents the polymer chain. "Allylic vinyl group," "allyl chain end," "vinyl chain end," "vinyl termination," "allylic vinyl group," and "vinyl terminated" are used interchangeably in the following description. The number of allyl chain ends, vinylidene chain ends, vinylene chain ends, and other unsaturated chain ends is determined using ^1H NMR at 120°C . using deuterated tetrachloroethane as the solvent on an at least 250 MHz NMR spectrometer, and in selected cases, confirmed by ^{13}C NMR. Resconi has reported proton and carbon assignments (neat perdeuterated tetrachloroethane used for proton spectra, while a 50:50 mixture of normal and perdeuterated tetrachloroethane was used for carbon spectra; all spectra were recorded at 100°C . on a BRUKER spectrometer operating at 500 MHz for proton and 125 MHz for carbon) for vinyl terminated oligomers in *J. American Chemical Soc.*, 114, 1992, pp. 1025-1032, that are useful herein. Allyl chain ends are reported as a molar percentage of the total number of moles of unsaturated groups (that is, the sum of allyl chain ends, vinylidene chain ends, vinylene chain ends, and the like).

A 3-alkyl chain end (where the alkyl is a C_1 to C_{38} alkyl), also referred to as a "3-alkyl vinyl end group" or a "3-alkyl vinyl termination," is represented by the formula:



where "...." represents the polyolefin chain and R^b is a C_1 to C_{38} alkyl group, or a C_1 to C_{20} alkyl group, such as methyl, ethyl, propyl, butyl, pentyl, hexyl, heptyl, octyl, nonyl, decyl, undecyl, dodecyl, and the like. The amount of 3-alkyl chain ends is determined using ^{13}C NMR as set out below.

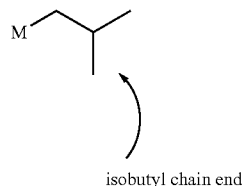
^{13}C NMR data is collected at 120°C . at a frequency of at least 100 MHz, using a BRUKER 400 MHz NMR spectrometer. A 90 degree pulse, an acquisition time adjusted to give a digital resolution between 0.1 and 0.12 Hz, at least a 10 second pulse acquisition delay time with continuous broadband proton decoupling using swept square wave modulation without gating is employed during the entire acquisition period. The spectra is acquired with time averaging to provide

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a signal to noise level adequate to measure the signals of interest. Samples are dissolved in tetrachloroethane- d_2 at concentrations between 10 wt % to 15 wt % prior to being inserted into the spectrometer magnet. Prior to data analysis, spectra are referenced by setting the chemical shift of the TCE solvent signal to 74.39 ppm. Chain ends for quantization were identified using the signals shown in the table below. N-butyl and n-propyl were not reported due to their low abundance (less than 5%) relative to the chain ends shown in the table below.

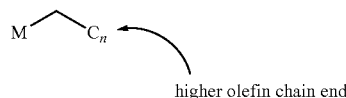
Chain End	^{13}C NMR Chemical Shift
P~i-Bu	23.5 to 25.5 and 25.8 to 26.3 ppm
E~i-Bu	39.5 to 40.2 ppm
P~Vinyl	41.5 to 43 ppm
E~Vinyl	33.9 to 34.4 ppm

The "allyl chain end to vinylidene chain end ratio" is defined to be the ratio of the percentage of allyl chain ends to the percentage of vinylidene chain ends. The "allyl chain end to vinylene chain end ratio" is defined to be the ratio of the percentage of allyl chain ends to the percentage of vinylene chain ends. Vinyl terminated macromonomers typically also have a saturated chain end. In polymerizations where propylene is present, the polymer chain may initiate growth in a propylene monomer, thereby generating an isobutyl chain end. An "isobutyl chain end" is defined to be an end or terminus of a polymer, represented as shown in the formula below:



where M represents the polymer chain. Isobutyl chain ends are determined according to the procedure set out in WO 2009/155471. The "isobutyl chain end to allylic vinyl group ratio" is defined to be the ratio of the percentage of isobutyl chain ends to the percentage of allyl chain ends. The "isobutyl chain end to alpha bromo carbon ratio" is defined to be the ratio of the percentage of isobutyl chain ends to the percentage of brominated chain ends (at about 34 ppm).

In polymerizations comprising C_4 or greater monomers (or "higher olefin" monomers), the saturated chain end may be a C_4 or greater (or "higher olefin") chain end, as shown in the formula below:



where M represents the polymer chain and n is an integer selected from 4 to 40. This is especially true when there is substantially no ethylene or propylene in the polymerization. In an ethylene/ C_4 or greater monomer copolymerization, the polymer chain may initiate growth in an ethylene monomer, thereby generating a saturated chain end which is an ethyl chain end. Mn (^1H NMR) is determined according to the

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following NMR method. ^1H NMR data is collected at either 25° C. or 120° C. (for purposes of the claims, 120° C. shall be used) in a 5 mm probe using a Varian spectrometer with a ^1H frequency of 250 MHz, 400 MHz, or 500 MHz (for the purpose of the claims, a proton frequency of 400 MHz is used). Data are recorded using a maximum pulse width of 45°, 8 seconds between pulses, and signal averaging 120 transients. Spectral signals are integrated and the number of unsaturation types per 1000 carbons is calculated by multiplying the different groups by 1000 and dividing the result by the total number of carbons. Mn is calculated by dividing the total number of unsaturated species into 14,000 and has units of g/mol. The chemical shift regions for the olefin types are defined to be between the following spectral regions.

Unsaturation Type	Region (ppm)	Number of hydrogens per structure
Vinyl	4.95-5.10	2
Vinylidene (VYD)	4.70-4.84	2
Vinylene	5.31-5.55	2
Trisubstituted	5.11-5.30	1

Unless otherwise stated, Mn (GPC) is determined using the GPC-DRI method described below; however, Nota Bene: for the purpose of the claims, Mn is determined by ^1H NMR. Mn, Mw, and Mz may be measured by using a Gel Permeation Chromatography (GPC) method using a High Temperature Size Exclusion Chromatograph (SEC, either from Waters Corporation or Polymer Laboratories), equipped with a differential refractive index detector (DRI). Molecular weight distribution (MWD) is Mw (GPC)/Mn (GPC). Experimental details, are described in: T. Sun, P. Brant, R. R. Chance, and W. W. Graessley, *Macromolecules*, Volume 34, Number 19, pp. 6812-6820, (2001) and references therein. Three Polymer Laboratories PLgel 10 mm Mixed-B columns are used. The nominal flow rate is 0.5 cm³/min and the nominal injection volume is 300 μL . The various transfer lines, columns and differential refractometer (the DRI detector) are contained in an oven maintained at 135° C. Solvent for the SEC experiment is prepared by dissolving 6 grams of butylated hydroxy toluene as an antioxidant in 4 liters of Aldrich reagent grade 1,2,4 trichlorobenzene (TCB). The TCB mixture is then filtered through a 0.7 μm glass pre-filter and subsequently through a 0.1 μm Teflon filter. The TCB is then degassed with an online degasser before entering the SEC. Polymer solutions are prepared by placing dry polymer in a glass container, adding the desired amount of TCB, then heating the mixture at 160° C. with continuous agitation for about 2 hours. All quantities are measured gravimetrically. The TCB densities used to express the polymer concentration in mass/volume units are 1.463 g/mL at 25° C. and 1.324 g/mL at 135° C. The injection concentration is from 1.0 to 2.0 mg/mL, with lower concentrations being used for higher molecular weight samples. Prior to running each sample the DRI detector and the injector are purged. Flow rate in the apparatus is then increased to 0.5 mL/minute and the DRI is allowed to stabilize for 8 to 9 hours before injecting the first sample. The concentration, c, at each point in the chromatogram is calculated from the baseline-subtracted DRI signal, I_{DRI} , using the following equation:

$$c = K_{DRI} I_{DRI} (dn/dc)$$

where K_{DRI} is a constant determined by calibrating the DRI and (dn/dc) is the refractive index increment for the system. The refractive index, $n=1.500$ for TCB at 135° C. and $\lambda=690$ nm. For purposes of this invention and the claims thereto, $(dn/dc)=0.104$ for propylene polymers and ethylene poly-

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mers, and 0.1 otherwise. Units of parameters used throughout this description of the SEC method are: concentration is expressed in g/cm³, molecular weight is expressed in g/mol, and intrinsic viscosity is expressed in dL/g.

The branching index ($g'_{(vis)}$) is calculated using the output of the SEC-DRI-LS-VIS method as follows. The average intrinsic viscosity, $[\eta]_{avg}$, of the sample is calculated by:

$$[\eta]_{avg} = \frac{\sum c_i [\eta]_i}{\sum c_i}$$

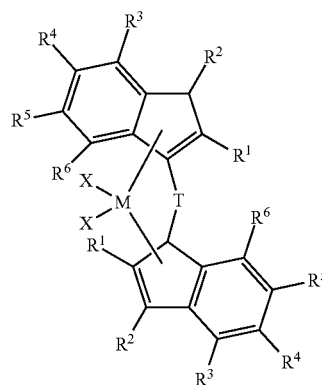
where the summations are over the chromatographic slices, i, between the integration limits.

The branching index $g'_{(vis)}$ is defined as:

$$g'_{vis} = \frac{[\eta]_{avg}}{k M_v^\alpha}$$

where, for purpose of this invention and claims thereto, $\alpha=0.695$ and $k=0.000579$ for linear ethylene polymers, $\alpha=0.705$ and $k=0.000262$ for linear propylene polymers, and $\alpha=0.695$ and $k=0.000181$ for linear butene polymers. M_v is the viscosity-average molecular weight based on molecular weights determined by LS analysis. See *Macromolecules*, 2001, 34, pp. 6812-6820 and *Macromolecules*, 2005, 38, pp. 7181-7183, for guidance on selecting a linear standard having similar molecular weight and comonomer content, and determining k coefficients and α exponents.

In an embodiment, the polyolefin is derived from a vinyl terminated propylene polymer. In an embodiment, the vinyl terminated propylene polymer is produced using a process comprising: contacting propylene, under polymerization conditions, with a catalyst system comprising an activator and at least one metallocene compound represented by the formula:



where:

M is hafnium or zirconium;

each X is, independently, selected from the group consisting of hydrocarbyl radicals having from 1 to 20 carbon atoms, hydrides, amides, alkoxides, sulfides, phosphides, halides, dienes, amines, phosphines, ethers, and a combination thereof, (two X's may form a part of a fused ring or a ring system);

each R¹ is, independently, a C₁ to C₁₀ alkyl group;

each R² is, independently, a C₁ to C₁₀ alkyl group;

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each R³ is hydrogen;

each R⁴, R⁵, and R⁶, is, independently, hydrogen or a substituted hydrocarbyl or unsubstituted hydrocarbyl group, or a heteroatom;

T is a bridging group;

further provided that any of adjacent R⁴, R⁵, and R⁶ groups may form a fused ring or multicenter fused ring system where the rings may be aromatic, partially saturated or saturated; and

obtaining a propylene polymer having at least 50% allyl chain ends (relative to total unsaturations), as described in co-pending U.S. Pat. No. 8,455,597, which is incorporated by reference in its entirety herein.

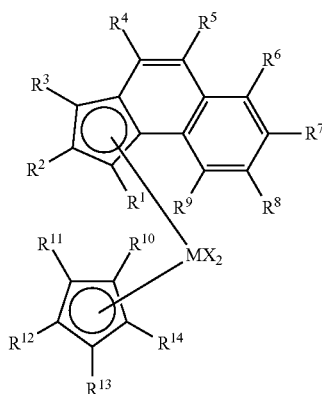
In an embodiment, the vinyl terminated propylene polymer is produced using a process comprising:

1) contacting:

a) one or more olefins with

b) a transition metal catalyst compound represented by the

formula:



wherein

M is hafnium or zirconium;

each X is, independently, selected from the group consisting of hydrocarbyl radicals having from 1 to 20 carbon atoms, hydrides, amides, alkoxides, sulfides, phosphides, halogens, dienes, amines, phosphines, ethers, or a combination thereof;

each R¹ and R³ are, independently, a C₁ to C₈ alkyl group;

each R², R⁴, R⁵, R⁶, R⁷, R⁸, R⁹, R¹⁰, R¹¹, R¹², R¹³, and R¹⁴ are, independently, hydrogen, or a substituted or unsubstituted hydrocarbyl group having from 1 to 8 carbon atoms, provided, however, that at least three of the R¹⁰-R¹⁴ groups are not hydrogen; and

2) obtaining vinyl terminated polymer having an Mn of 300 g/mol or more and at least 30% allyl chain ends (relative to total unsaturation), as described in U.S. Pat. No. 8,318,998, which is incorporated by reference in its entirety herein.

In an embodiment, the polyolefin chain is derived from a higher olefin copolymer comprising allyl chain ends. In an embodiment, the higher olefin copolymer comprising allyl chain ends has an Mn of 300 g/mol or more (measured by ¹H NMR) comprising:

(i) from about 20 mol % to about 99.9 mol % of at least one C₅ to C₄₀ higher olefin;

(ii) from about 0.1 mol % to about 80 mol % of propylene; and wherein the higher olefin copolymer has at least 40% allyl chain ends, as described in U.S. Pat. No. 8,399,724, which is incorporated by reference in its entirety herein.

In an embodiment, the polyolefin chain is derived from a vinyl terminated branched polyolefin. In an embodiment, the

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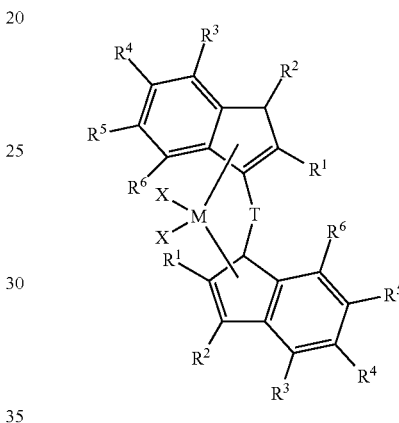
vinyl terminated branched polyolefin has an Mn (¹H NMR) of 7,500 to 60,000 g/mol, comprising one or more alpha olefin derived units comprising ethylene and/or propylene, and having:

(i) 50% or greater allyl chain ends, relative to total number of unsaturated chain ends; and

(ii) a g'_{vis} of 0.90 or less, as described in U.S. Publication No. 2012-0245299, which is incorporated by reference in its entirety herein.

In an embodiment, the polyolefin chain is derived from a vinyl terminated branched polyolefin produced by a process for polymerization, comprising:

(i) contacting, at a temperature greater than 35° C., one or more monomers comprising ethylene and/or propylene, with a catalyst system comprising a metallocene catalyst compound and an activator, wherein the metallocene catalyst compound is represented by the following formula:



where:

M is selected from the group consisting of zirconium or hafnium;

each X is, independently, selected from the group consisting of hydrocarbyl radicals having from 1 to 20 carbon atoms, hydrides, amides, alkoxides, sulfides, phosphides, halides, dienes, amines, phosphines, ethers, and a combination thereof, (two X's may form a part of a fused ring or a ring system);

each R¹, R², R³, R⁴, R⁵, and R⁶, is, independently, hydrogen or a substituted or unsubstituted hydrocarbyl group, a heteroatom or heteroatom containing group;

further provided that any two adjacent R groups may form a fused ring or multicenter fused ring system where the rings may be aromatic, partially saturated or saturated; further provided that any of adjacent R⁴, R⁵, and R⁶ groups may form a fused ring or multicenter fused ring system where the rings may be aromatic, partially saturated or saturated;

T is a bridging group represented by the formula (Ra)₂J, where J is one or more of C, Si, Ge, N or P, and each Ra is, independently, hydrogen, halogen, C₁ to C₂₀ hydrocarbyl or a C₁ to C₂₀ substituted hydrocarbyl, provided that at least one R³ is a substituted or unsubstituted phenyl group, if any of R¹, R², R⁴, R⁵, or R⁶ are not hydrogen;

(ii) converting at least 50 mol % of the monomer to polyolefin; and

(iii) obtaining a branched polyolefin having greater than 50% allyl chain ends, relative to total unsaturated chain ends and a Tm of 60° C. or more, as described in U.S. Publication No. 2012-0245299, which is incorporated by reference in its entirety herein.

In an embodiment of the invention, the polyolefin is derived from a vinyl terminated ethylene polymer, preferably a vinyl terminated polyethylene (preferably in particulate form) having:

(a) at least 60% allyl chain ends (preferably at least 65%, preferably at least 70%, preferably at least 75%, preferably at least 80%, preferably at least 85%, preferably at least 90%, preferably at least 95%, preferably at least 96%, preferably at least 97%, preferably at least 98%, preferably at least 99%, or preferably at least 100%);

(b) a molecular weight distribution of less than or equal to 4.0 (preferably less than or equal to 3.8, preferably less than or equal to 3.5, preferably less than or equal to 3.2, preferably less than or equal to 3.0, preferably less than or equal to 2.8, or preferably less than or equal to 2.5);

(c) an Mn (^1H NMR) of at least 20,000 g/mol (preferably at least 25,000 g/mol, preferably at least 30,000 g/mol, preferably at least 40,000 g/mol, preferably at least 50,000 g/mol, and, optionally, less than 125,000 g/mol, preferably less than 120,000, or preferably less than 110,000);

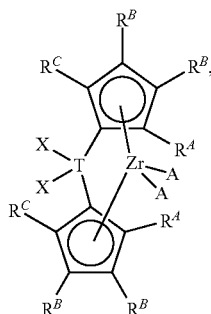
(d) optionally, an Mn (GPC)/Mn (^1H NMR) in the range of from about 0.8 to about 1.2 (preferably from about 0.9 to about 1.1, preferably from about 0.95 to about 1.1); and

(e) optionally, a $g'_{(vis)}$ of greater than 0.95 (preferably greater than 0.96, preferably greater than 0.98, preferably greater than 0.98, and, optionally, preferably less than or equal to 1.0).

Preferably, the vinyl terminated ethylene polymers are prepared by a process comprising:

(a) contacting ethylene with a supported metallocene catalyst system;

wherein the supported catalyst system comprises: (i) a support material; (ii) an activator having from about 1 wt % to about 14 wt % trimethylaluminum, based on the weight of the activator; (iii) a metallocene compound represented by the formula:



wherein: T is Si or Ge; each R^A is a C_1 to C_{20} substituted or unsubstituted hydrocarbyl group; each R^B is, independently, H, or a C_1 to C_8 substituted or unsubstituted hydrocarbyl group, or a group represented by the formula $-\text{CH}_2\text{R}^x$; wherein R^x is a C_1 to C_{20} substituted or unsubstituted hydrocarbyl group, provided that at least one R^B is methyl or a group represented by the formula $-\text{CH}_2\text{R}^x$; each R^C is, independently, H or a C_1 to C_{20} substituted or unsubstituted hydrocarbyl group; each A is independently selected from the group consisting of C_1 to C_{20} substituted or unsubstituted hydrocarbyl groups, hydrides, amides, amines, alkoxides, sulfides, phosphides, halides, dienes, phosphines, and ethers; each X is, independently, hydrogen, halogen, or a C_1 to C_{20} hydrocarbyl, and two X groups can form a cyclic structure including aromatic, partially saturated, or saturated cyclic or

fused ring system; further provided that any of adjacent R^A , R^B , and/or R^C groups may form a fused ring or multicenter fused ring systems, where the rings may be substituted or unsubstituted, and may be aromatic, partially unsaturated, or unsaturated;

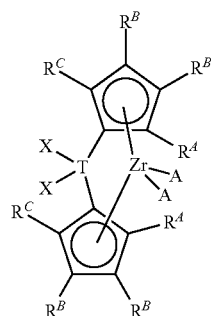
(b) obtaining a vinyl terminated polyethylene having: (i) at least 60% allyl chain ends; (ii) a molecular weight distribution of less than or equal to 4.0; and (iii) a Mn (^1H NMR) of at least 20,000 g/mol. Preferably, the vinyl terminated ethylene polymers are made according the process (and using the catalyst systems) described in (U.S. Ser. No. 61/704,606, filed Sep. 24, 2012, entitled Production of Vinyl Terminated Polyethylene Using Supported Catalyst System).

In an embodiment of the invention, the polyolefin is derived from a vinyl terminated ethylene polymer, preferably a vinyl terminated polyethylene having: (i) at least 50% allyl chain ends (preferably 60%, 70%, 80%, 90%, 95%, 96%, 97%, 98%, 99%, or 100%); (ii) a molecular weight distribution of less than or equal to 4.0 (preferably less than or equal to 3.8, 3.6, 3.5, 3.4, 3.2, 3.0, 2.8, or 2.5); (iii) a $g'_{(vis)}$ of 0.95 or less (preferably less than 0.93, 0.90, 0.88, or 0.85); (iv) an Mn (^1H NMR) of at least 7,000 g/mol (preferably at least 10,000 g/mol, 15,000 g/mol, 20,000 g/mol, 25,000 g/mol, 30,000 g/mol, 45,000 g/mol, 55,000 g/mol, 65,000 g/mol, or 85,000 g/mol, and, optionally, less than 125,000 g/mol); and (v) a Mn (GPC)/Mn (^1H NMR) in the range of from about 0.8 to about 1.2 (preferably from 0.85 to 1.15, 0.90 to 1.10, and 0.95 to 1.00). Preferably, the vinyl terminated ethylene polymers are produced by a process comprising:

(a) contacting ethylene with a metallocene catalyst system; wherein the catalyst system comprises:

(i) an ionizing activator;

(ii) a metallocene compound represented by the formula:



wherein T is Si or Ge; each R^A is a C_1 to C_{20} substituted or unsubstituted hydrocarbyl group; each R^B is, independently, H or a C_1 to C_8 substituted or unsubstituted hydrocarbyl group, or a group represented by the formula $-\text{CH}_2\text{R}^x$; wherein R^x is a C_1 to C_{20} substituted or unsubstituted hydrocarbyl group, provided that at least one R^B is methyl or a group represented by the formula $-\text{CH}_2\text{R}^x$; each R^C is, independently, H or a C_1 to C_{20} substituted or unsubstituted hydrocarbyl group; each A is independently selected from the group consisting of C_1 to C_{20} substituted or unsubstituted hydrocarbyl groups, hydrides, amides, amines, alkoxides, sulfides, phosphides, halides, dienes, phosphines, and ethers; each X is, independently, hydrogen, halogen, or a C_1 to C_{20} hydrocarbyl, and two X groups can form a cyclic structure including aromatic, partially saturated, or saturated cyclic or fused ring system; further provided that any of adjacent R^A , R^B , and/or R^C groups may form a fused ring or multicenter

fused ring systems, where the rings may be substituted or unsubstituted, and may be aromatic, partially unsaturated or unsaturated;

(b) obtaining a vinyl terminated polyethylene having: (i) at least 50% allyl chain ends; (ii) a molecular weight distribution of less than or equal to 4.0; (iii) a g'_{vis} of 0.95 or less; (iv) a Mn (^1H NMR) of at least 7,000 g/mol; and (v) a Mn (GPC)/Mn (^1H NMR) in the range of from about 0.8 to about 1.2. Preferably, the vinyl terminated ethylene polymers are made according to the process (and using the catalyst systems) described in (U.S. Ser. No. 61/704,604, filed Sep. 24, 2012, entitled Production of Vinyl Terminated Polyethylene).

In any of the polymerizations described herein, the activator may be an alumoxane, an aluminum alkyl, a stoichiometric activator (also referred to as an ionizing activator), which may be neutral or ionic, and/or a conventional-type cocatalyst, unless otherwise stated. Preferred activators typically include alumoxane compounds, modified alumoxane compounds, stoichiometric activators, and ionizing anion precursor compounds that abstract one reactive, σ -bound, metal ligand making the metal complex cationic, and providing a charge-balancing noncoordinating or weakly coordinating anion.

Alumoxane Activators

In an embodiment of the invention, alumoxane activators are utilized as an activator in the catalyst composition, preferably methylalumoxane (MAO), modified methylalumoxane (MMAO), ethylalumoxane, and/or isobutylalumoxane. Preferably, the activator is a TMA-depleted activator (where TMA means trimethylaluminum). Any method known in the art to remove TMA may be used. For example, to produce a TMA-depleted activator, a solution of alumoxane (such as methylalumoxane), for example, 30 wt % in toluene may be diluted in toluene and the aluminum alkyl (such as TMA in the case of MAO) is removed from the solution, for example, by combination with trimethylphenol and filtration of the solid. In such embodiments, the TMA-depleted activator comprises from about 1 wt % to about 14 wt % trimethylaluminum (preferably less than 13 wt %, preferably less than 12 wt %, preferably less than 10 wt %, preferably less than 5 wt %, or preferably 0 wt %, or, optionally, greater than 0 wt % or greater than 1 wt %).

Stoichiometric Activators

The catalyst systems useful herein may comprise one or more stoichiometric activators. A stoichiometric activator is a non-alumoxane compound which when combined in a reaction with the catalyst compound (such as a metallocene compound) forms a catalytically active species, typically at molar ratios of stoichiometric activator to metallocene compound of 10:1 or less (preferably 5:1, more preferably 2:1, or even more preferably 1:1); however, it is within the scope of this invention to use a molar ratio of stoichiometric activator to metallocene compound of greater than 10:1 as well. Useful stoichiometric (or non-alumoxane) activator-to-catalyst ratios range from 0.5:1 to 10:1, preferably 1:1 to 5:1, although ranges of from 0.1:1 to 100:1, alternately from 0.5:1 to 200:1, alternately from 1:1 to 500:1 alternately from 1:1 to 1000:1, may be used.

Stoichiometric activators are non-alumoxane compounds which may be neutral or ionic, such as tri (n-butyl) ammonium tetrakis (pentafluorophenyl) borate, a tris perfluorophenyl boron metalloid precursor, or a tris perfluoronaphthyl boron metalloid precursor, polyhalogenated heteroborane anions (WO 98/43983), boric acid (U.S. Pat. No. 5,942,459), or a combination thereof. It is also within the scope of this invention to use stoichiometric activators alone or in combination with alumoxane or modified alumoxane activators.

Neutral Stoichiometric Activators

Examples of neutral stoichiometric activators include tri-substituted boron, tellurium, aluminum, gallium, and indium, or mixtures thereof. The three substituent groups are each independently selected from alkyls, alkenyls, halogens, substituted alkyls, aryls, arylhalides, alkoxy, and halides. Preferably, the three groups are independently selected from halogen, mono or multicyclic (including halosubstituted) aryls, alkyls, and alkenyl compounds, and mixtures thereof, preferred are alkenyl groups having 1 to 20 carbon atoms, alkyl groups having 1 to 20 carbon atoms, alkoxy groups having 1 to 20 carbon atoms and aryl groups having 3 to 20 carbon atoms (including substituted aryls). More preferably, the three groups are alkyls having 1 to 4 carbon groups, phenyl, naphthyl, or mixtures thereof. Even more preferably, the three groups are halogenated, preferably fluorinated, aryl groups. Preferably, the neutral stoichiometric activator is tris perfluorophenyl boron or tris perfluoronaphthyl boron.

Ionic Stoichiometric Activators

Ionic stoichiometric activators may contain an active proton, or some other cation associated with, but not coordinated to, or only loosely coordinated to, the remaining anion of the activator. Such compounds and the like are described in EP 0 570 982 A; EP 0 520 732 A; EP 0 495 375 A; EP 0 500 944 B1; EP 0 277 003 A; EP 0 277 004 A; U.S. Pat. Nos. 5,153,157; 5,198,401; 5,066,741; 5,206,197; 5,241,025; and 5,384,299; 5,502,124; all of which are herein fully incorporated by reference.

Ionic stoichiometric activators comprise a cation, which is preferably a Bronsted acid capable of donating a proton, and a compatible non-coordinating anion. Preferably, the anion is relatively large (bulky), capable of stabilizing the catalytically active species (preferably a group 4 catalytically active species) which is formed when the catalyst (such as a metallocene compound) and the stoichiometric activator are combined. Preferably, the anion will be sufficiently labile to be displaced by olefinic, diolefinic, and acetylenically unsaturated substrates or other neutral Lewis bases, such as ethers, amines, and the like. Two classes of useful compatible non-coordinating anions have been disclosed in EP 0 277,003 A, and EP 0 277,004 A: 1) anionic coordination complexes comprising a plurality of lipophilic radicals covalently coordinated to and shielding a central charge-bearing metal or metalloid core; and 2) anions comprising a plurality of boron atoms such as carboranes, metallacarboranes, and boranes.

Ionic stoichiometric activators comprise an anion, preferably a non-coordinating anion. The term "non-coordinating anion" (NCA) means an anion which either does not coordinate to said cation or which is only weakly coordinated to said cation thereby remaining sufficiently labile to be displaced by a neutral Lewis base. "Compatible" non-coordinating anions are those which are not degraded to neutrality when the initially formed complex decomposes. Further, the anion will not transfer an anionic substituent or fragment to the cation so as to cause it to form a neutral four coordinate metallocene compound and a neutral by-product from the anion. Non-coordinating anions useful in accordance with this invention are those that are compatible, stabilize the catalyst (such as metallocene) cation in the sense of balancing its ionic charge at +1, yet retain sufficient lability to permit displacement by an ethylenically or acetylenically unsaturated monomer during polymerization.

In a preferred embodiment of this invention, the ionic stoichiometric activators are represented by the following formula (I):



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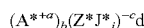
wherein $(Z)_d^+$ is the cation component and A^{d-} is the anion component; where Z is (L-H) or a reducible Lewis Acid, L is an neutral Lewis base; H is hydrogen; (L-H)⁺ is a Bronsted acid; A^{d-} is a non-coordinating anion having the charge d-; and d is an integer from 1 to 3.

When Z is (L-H) such that the cation component is $(L-H)_d^+$, the cation component may include Bronsted acids such as protonated Lewis bases capable of protonating a moiety, such as an alkyl or aryl, from the bulky ligand metallocene containing transition metal catalyst precursor, resulting in a cationic transition metal species. Preferably, the activating cation $(L-H)_d^+$ is a Bronsted acid, capable of donating a proton to the transition metal catalytic precursor resulting in a transition metal cation, including ammoniums, oxoniums, phosphoniums, silyliums, and mixtures thereof, preferably ammoniums of methylamine, aniline, dimethylamine, diethylamine, N-methylaniline, diphenylamine, trimethylamine, triethylamine, N,N-dimethylaniline, methyl diphenylamine, pyridine, p-bromo N,N-dimethylaniline, p-nitro-N,N-dimethylaniline, phosphoniums from triethylphosphine, triphenylphosphine, and diphenylphosphine, oxoniums from ethers, such as dimethyl ether diethyl ether, tetrahydrofuran, and dioxane, sulfoniums from thioethers, such as diethyl thioethers and tetrahydrothiophene, and mixtures thereof.

When Z is a reducible Lewis acid, $(Z)_d^+$ is preferably represented by the formula: $(Ar_3C)^+$, where Ar is aryl or aryl substituted with a heteroatom, a C₁ to C₄₀ hydrocarbyl, or a substituted C₁ to C₄₀ hydrocarbyl, preferably $(Z)_d^+$ is represented by the formula: $(Ph_3C)^+$, where Ph is phenyl or phenyl substituted with a heteroatom, a C₁ to C₄₀ hydrocarbyl, or a substituted C₁ to C₄₀ hydrocarbyl. In a preferred embodiment, the reducible Lewis acid is triphenyl carbenium.

The anion component A^{d-} includes those having the formula $[M^{k+}Q_n]^{d-}$ wherein k is 1, 2, or 3; n is 1, 2, 3, 4, 5, or 6, preferably 3, 4, 5, or 6; n=k=d; M is an element selected from group 13 of the Periodic Table of the Elements, preferably boron or aluminum; and each Q is independently a hydride, bridged or unbridged dialkylamido, halide, alkoxide, aryloxide, hydrocarbyl, substituted hydrocarbyl, halocarbyl, substituted halocarbyl, and halosubstituted-hydrocarbyl radicals, said Q having up to 20 carbon atoms with the proviso that in not more than one occurrence is Q a halide, and two Q groups may form a ring structure. Preferably, each Q is a fluorinated hydrocarbyl group having 1 to 20 carbon atoms, more preferably each Q is a fluorinated aryl group, and most preferably each Q is a pentafluorophenyl group. Examples of suitable A^{d-} components also include diboron compounds as disclosed in U.S. Pat. No. 5,447,895, which is fully incorporated herein by reference.

In other embodiments of this invention, the ionic stoichiometric activator may be an activator comprising expanded anions, represented by the formula:



wherein A^* is a cation having charge +a; Z^* is an anion group of from 1 to 50 atoms not counting hydrogen atoms, further containing two or more Lewis base sites; J^* independently each occurrence is a Lewis acid coordinated to at least one Lewis base site of Z^* ; and, optionally, two or more such J^* groups may be joined together in a moiety having multiple Lewis acid functionality; j is a number from 2 to 12; and a, b, c, and d are integers from 1 to 3, with the proviso that axb is equal to $cx d$. Examples of such activators comprising expandable anions may be found in U.S. Pat. No. 6,395,671, which is fully incorporated herein by reference.

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Examples of ionic stoichiometric activators useful in the catalyst system of this invention are:

trimethylammonium tetraphenylborate, triethylammonium tetraphenylborate, tripropylammonium tetraphenylborate, tri(n-butyl)ammonium tetraphenylborate, tri(t-butyl)ammonium tetraphenylborate, N,N-dimethylanilinium tetraphenylborate, N,N-diethylanilinium tetraphenylborate, N,N-dimethyl-(2,4,6-trimethylanilinium) tetraphenylborate, tropillium tetraphenylborate, triphenylcarbenium tetraphenylborate, triphenylphosphonium tetraphenylborate, triethylsilylium tetraphenylborate, benzene(diazonium) tetraphenylborate, trimethylammonium tetrakis(pentafluorophenyl)borate, triethylammonium tetrakis(pentafluorophenyl)borate, tripropylammonium tetrakis(pentafluorophenyl)borate, tri(n-butyl)ammonium tetrakis(pentafluorophenyl)borate, tri(sec-butyl)ammonium tetrakis(pentafluorophenyl)borate, N,N-dimethylanilinium tetrakis(pentafluorophenyl)borate, N,N-diethylanilinium tetrakis(pentafluorophenyl)borate, N,N-dimethyl-(2,4,6-trimethylanilinium) tetrakis(pentafluorophenyl)borate, tropillium tetrakis(pentafluorophenyl)borate, triphenylcarbenium tetrakis(pentafluorophenyl)borate, triphenylphosphonium tetrakis(pentafluorophenyl)borate, triethylsilylium tetrakis(pentafluorophenyl)borate, benzene(diazonium) tetrakis(pentafluorophenyl)borate, trimethylammonium tetrakis-(2,3,4,6-tetrafluorophenyl)borate, triethylammonium tetrakis-(2,3,4,6-tetrafluorophenyl)borate, tripropylammonium tetrakis-(2,3,4,6-tetrafluorophenyl)borate, tri(n-butyl)ammonium tetrakis-(2,3,4,6-tetrafluorophenyl)borate, dimethyl(t-butyl)ammonium tetrakis-(2,3,4,6-tetrafluorophenyl)borate, N,N-dimethylanilinium tetrakis-(2,3,4,6-tetrafluorophenyl)borate, N,N-diethylanilinium tetrakis-(2,3,4,6-tetrafluorophenyl)borate, N,N-dimethyl-(2,4,6-trimethylanilinium)tetrakis-(2,3,4,6-tetrafluorophenyl)borate, tropillium tetrakis-(2,3,4,6-tetrafluorophenyl)borate, triphenylcarbenium tetrakis-(2,3,4,6-tetrafluorophenyl)borate, triphenylphosphonium tetrakis-(2,3,4,6-tetrafluorophenyl)borate, triethylsilylium tetrakis-(2,3,4,6-tetrafluorophenyl)borate, benzene(diazonium)tetrakis-(2,3,4,6-tetrafluorophenyl)borate, trimethylammonium tetrakis(perfluoronaphthyl)borate, triethylammonium tetrakis(perfluoronaphthyl)borate, tripropylammonium tetrakis(perfluoronaphthyl)borate, tri(n-butyl)ammonium tetrakis(perfluoronaphthyl)borate, tri(t-butyl)ammonium tetrakis(perfluoronaphthyl)borate, N,N-dimethylanilinium tetrakis(perfluoronaphthyl)borate, N,N-diethylanilinium tetrakis(perfluoronaphthyl)borate, N,N-dimethyl-(2,4,6-trimethylanilinium) tetrakis(perfluoronaphthyl)borate, tropillium tetrakis(perfluoronaphthyl)borate, triphenylcarbenium tetrakis(perfluoronaphthyl)borate, triphenylphosphonium tetrakis(perfluoronaphthyl)borate, triethylsilylium tetrakis(perfluoronaphthyl)borate, benzene(diazonium) tetrakis(perfluoronaphthyl)borate, trimethylammonium tetrakis(perfluorobiphenyl)borate, triethylammonium tetrakis(perfluorobiphenyl)borate, tripropylammonium tetrakis(perfluorobiphenyl)borate, tri(n-butyl)ammonium tetrakis(perfluorobiphenyl)borate, tri(t-butyl)ammonium tetrakis(perfluorobiphenyl)borate, N,N-dimethylanilinium tetrakis(perfluorobiphenyl)borate, N,N-diethylanilinium tetrakis(perfluorobiphenyl)borate, N,N-dimethyl-(2,4,6-trimethylanilinium) tetrakis(perfluorobiphenyl)borate, tropillium tetrakis(perfluorobiphenyl)borate, triphenylcarbenium tetrakis(perfluorobiphenyl)borate, triphenylphosphonium tetrakis(perfluorobiphenyl)borate, triethylsilylium tetrakis(perfluorobiphenyl)borate, benzene

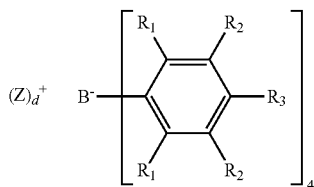
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(diazonium) tetrakis(perfluorobiphenyl)borate, trimethylammonium tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, triethylammonium tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, tripropylammonium tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, tri(n-butyl)ammonium tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, tri(t-butyl)ammonium tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, N,N-dimethylanilinium tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, N,N-diethylanilinium tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, N,N-dimethyl-(2,4,6-trimethylanilinium)tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, tropillium tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, triphenylcarbenium tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, triphenylphosphonium tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, triethylsilylium tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, benzene(diazonium)tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, and dialkyl ammonium salts such as: di(isopropyl)ammonium tetrakis(pentafluorophenyl)borate, and dicyclohexylammonium tetrakis(pentafluorophenyl)borate; and additional tri-substituted phosphonium salts such as tri(o-tolyl)phosphonium tetrakis(pentafluorophenyl)borate, and tri(2,6-dimethylphenyl)phosphonium tetrakis(pentafluorophenyl)borate.

Most preferably, the ionic stoichiometric activator is N,N-dimethylanilinium tetrakis(perfluoronaphthyl)borate, N,N-dimethylanilinium tetrakis(perfluorobiphenyl)borate, N,N-dimethylanilinium tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, triphenylcarbenium tetrakis(perfluoronaphthyl)borate, triphenylcarbenium tetrakis(perfluorobiphenyl)borate, triphenylcarbenium tetrakis(3,5-bis(trifluoromethyl)phenyl)borate, or triphenylcarbenium tetrakis(perfluorophenyl)borate.

Bulky Ionic Stoichiometric Activators

"Bulky activator" as used herein refers to ionic stoichiometric activators represented by the formula:



where:

each R₁ is, independently, a halide, preferably a fluoride; each R₂ is, independently, a halide, a C₆ to C₂₀ substituted aromatic hydrocarbyl group or a siloxy group of the formula —O—Si—R_a, where R_a is a C₁ to C₂₀ substituted or

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unsubstituted hydrocarbyl or hydrocarbylsilyl group (preferably R₂ is a fluoride or a perfluorinated phenyl group); each R₃ is a halide, C₆ to C₂₀ substituted aromatic hydrocarbyl group or a siloxy group of the formula —O—Si—R_a, where R_a is a C₁ to C₂₀ substituted or unsubstituted hydrocarbyl or hydrocarbylsilyl group (preferably R₃ is a fluoride or a C₆ perfluorinated aromatic hydrocarbyl group); wherein R₂ and R₃ can form one or more saturated or unsaturated, substituted or unsubstituted rings (preferably R₂ and R₃ form a perfluorinated phenyl ring); (Z)_d⁺ is the cation component, where Z is (L-H) or a reducible Lewis Acid; L is a neutral Lewis base; H is hydrogen; (L-H)⁺ is a Brønsted acid; and d is an integer from 1 to 3;

wherein the boron anion component has a molecular weight of greater than 1020 g/mol; and wherein at least three of the substituents on the B atom each have a molecular volume of greater than 250 cubic Å, alternately greater than 300 cubic Å, or alternately greater than 500 cubic Å.

"Molecular volume" is used herein as an approximation of spatial steric bulk of an activator molecule in solution. Comparison of substituents with differing molecular volumes allows the substituent with the smaller molecular volume to be considered "less bulky" in comparison to the substituent with the larger molecular volume. Conversely, a substituent with a larger molecular volume may be considered "more bulky" than a substituent with a smaller molecular volume.

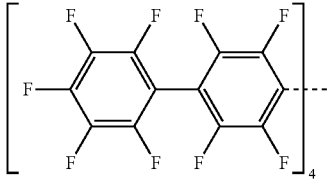
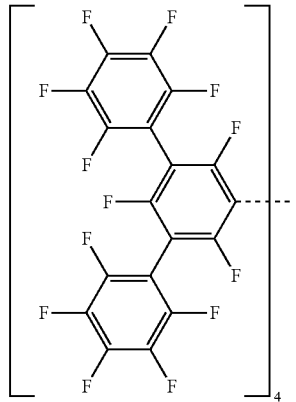
Molecular volume may be calculated as reported in "A Simple 'Back of the Envelope' Method for Estimating the Densities and Molecular Volumes of Liquids and Solids," Journal of Chemical Education, Vol. 71, No. 11, November 1994, pp. 962-964. Molecular volume (MV), in units of cubic Å, is calculated using the formula: MV=8.3V_s, where V_s is the scaled volume. V_s is the sum of the relative volumes of the constituent atoms, and is calculated from the molecular formula of the substituent using the following table of relative volumes. For fused rings, the V_s is decreased by 7.5% per fused ring.

Element	Relative Volume
H	1
1st short period, Li to F	2
2nd short period, Na to Cl	4
1st long period, K to Br	5
2nd long period, Rb to I	7.5
3rd long period, Cs to Bi	9

Exemplary bulky substituents of activators suitable herein and their respective scaled volumes and molecular volumes are shown in the table below. The dashed bonds indicate binding to boron, as in the general formula above.

Activator	Structure of boron substituents	Molecular Formula of each substituent	MV Per subst. V _s	Total MV (Å ³)
Dimethylanilinium tetrakis(perfluoronaphthyl)borate		C ₁₀ F ₇	34	261 1044

-continued

Activator	Structure of boron substituents	Molecular Formula of each substituent	V_s	MV Per subst. (\AA^3)	Total MV (\AA^3)
Dimethylanilinium tetrakis(perfluorobiphenyl)borate		C_{12}F_9	42	349	1396
[4-tButyl-PhNMe ₂ H] [(C ₆ F ₅ (C ₆ F ₅) ₂) ₄ B]		$\text{C}_{18}\text{F}_{13}$	62	515	2060

Exemplary bulky ionic stoichiometric activators useful in catalyst systems herein include: trimethylammonium tetrakis(perfluoronaphthyl)borate, triethylammonium tetrakis(perfluoronaphthyl)borate, tripropylammonium tetrakis(perfluoronaphthyl)borate, tri(n-butyl)ammonium tetrakis(perfluoronaphthyl)borate, tri(t-butyl)ammonium tetrakis(perfluoronaphthyl)borate, N,N-dimethylanilinium tetrakis(perfluoronaphthyl)borate, N,N-diethylanilinium tetrakis(perfluoronaphthyl)borate, N,N-dimethyl-(2,4,6-trimethylanilinium)tetrakis(perfluoronaphthyl)borate, tropillium tetrakis(perfluoronaphthyl)borate, triphenylcarbenium tetrakis(perfluoronaphthyl)borate, triphenylphosphonium tetrakis(perfluoronaphthyl)borate, triethylsilylium tetrakis(perfluoronaphthyl)borate, benzene(diazonium)tetrakis(perfluoronaphthyl)borate, trimethylammonium tetrakis(perfluorobiphenyl)borate, triethylammonium tetrakis(perfluorobiphenyl)borate, tripropylammonium tetrakis(perfluorobiphenyl)borate, tri(n-butyl)ammonium tetrakis(perfluorobiphenyl)borate, tri(t-butyl)ammonium tetrakis(perfluorobiphenyl)borate, N,N-dimethylanilinium tetrakis(perfluorobiphenyl)borate, N,N-diethylanilinium tetrakis(perfluorobiphenyl)borate, N,N-dimethyl-(2,4,6-trimethylanilinium)tetrakis(perfluorobiphenyl)borate, tropillium tetrakis(perfluorobiphenyl)borate, triphenylcarbenium tetrakis(perfluorobiphenyl)borate, triphenylphosphonium tetrakis(perfluorobiphenyl)borate, triethylsilylium tetrakis(perfluorobiphenyl)borate, benzene(diazonium)tetrakis(perfluorobiphenyl)borate, [4-t-butyl-PhNMe₂H][(C₆F₅(C₆F₅)₂)₄B], (where Ph is phenyl and Me is methyl), and the types disclosed in U.S. Pat. No. 7,297,653.

In another embodiment of this invention, an activation method using ionic compounds not containing an active proton but capable of producing a bulky ligand metallocene catalyst cation and their non-coordinating anion are also contemplated, and are described in EP 0 426 637 A, EP 0 573 403 A, and U.S. Pat. No. 5,387,568, which are all herein incorporated by reference.

In another embodiment of this invention, inventive processes also can employ stoichiometric activator compounds that are initially neutral Lewis acids but form a cationic metal complex and a noncoordinating anion, or a zwitterionic complex upon reaction with the metallocene compounds. For example, tris(pentafluorophenyl) boron or aluminum may act to abstract a hydrocarbyl or hydride ligand to yield an invention cationic metal complex and stabilizing noncoordinating anion, see EP 0 427 697 A and EP 0 520 732 A for illustrations of analogous group 4 metallocene compounds. Also, see the methods and compounds of EP 0 495 375 A. For formation of zwitterionic complexes using analogous group 4 compounds, see U.S. Pat. Nos. 5,624,878; 5,486,632; and 5,527,929.

In another embodiment of this invention, another suitable ionic stoichiometric activator comprises a salt of a cationic oxidizing agent and a noncoordinating, compatible anion represented by the formula:



wherein X^{e+} is a cationic oxidizing agent having a charge of $e+$; e is 1, 2, or 3; A^{d-} is a non-coordinating anion having the charge $d-$; and d is 1, 2, or 3. Examples of X^{e+} include: ferrocenium, hydrocarbyl-substituted ferrocenium, Ag^+ , or Pb^{+2} . Preferred embodiments of A^{d-} are those anions previously defined with respect to the Bronsted acid containing activators, especially tetrakis(pentafluorophenyl)borate.

Activator Combinations

It is within the scope of this invention that metallocene compounds can be combined with one or more activators or activation methods described above. For example, a combination of activators have been described in U.S. Pat. Nos. 5,153,157; 5,453,410; European Publication No. EP 0 573 120 B1; PCT Publication Nos. WO 94/07928; and WO 95/14044. These documents all discuss the use of an alumoxane in combination with a stoichiometric activator.

In another embodiment, the vinyl terminated macromonomer may be a vinyl terminated ethylene macromonomer. In some embodiments, a phenoxyimine-based catalyst (a Mitsui FI catalyst) or a pyrroleimine-based catalyst (a Mitsui PI catalyst) can be used to prepare the vinyl terminated ethylene macromonomer. These catalysts comprise (a) a transition metal (preferably Ti) compound having phenoxyimine or pyrroleimine as a ligand, and (b) one or more kind(s) of compound selected from (b-1) an organic metal compound, (b-2) an organic aluminumoxy compound, and (b-3) a compound that reacts with the transition metal compound (a) to form an ion pair, as described in JP-A-2001-72706, JP-A-2002-332312, JP-A-2003-313247, JP-A-2004-107486, and JP-A-2004-107563. Herein, as the transition metal contained in the transition metal compound, the transition metal of Groups 3 to 11 in the periodic table can be used. Preferred catalysts to prepare the vinyl terminated ethylene macromonomer include those described in U.S. Pat. No. 7,795,347, specifically at column 16, line 56 et seq. in Formula (XI).

In another embodiment, the vinyl terminated macromonomer may be a vinyl terminated isotactic polypropylene or a vinyl terminated polyethylene as disclosed in U.S. Pat. Nos. 6,444,773; 6,555,635; 6,147,180; 6,660,809; 6,750,307; 6,774,191; 6,169,154; and EP 0 958 309, which are incorporated by reference herein.

In a preferred embodiment, any vinyl terminated macromonomer described herein can be fractionated or distilled by any means known in the art and one or more of the fractions may be used in the invention described herein. Preferred fractions typically have a narrow Mw/Mn, such as less than 1.5, preferably 1.4 or less, preferably 1.3 or less, preferably 1.2 or less. Alternately the Mw/Mn is from 1 to 1.4, preferably 1.05 to 1.3, preferably 1.1 to 1.2.

In another embodiment of the invention, the fractions have a narrow boiling point range (as determined by ASTM D86) of less than 70° C., preferably less than 60° C., preferably less than 50° C., preferably less than 40° C., preferably less than 30° C., preferably less than 20° C., preferably less than 10° C.

In a preferred embodiment of the invention, the vinyl terminated macromonomer injected into a gas chromatograph column to determine the optimum cut points for the fractionation.

In a preferred embodiment, the fractions may be obtained by separation of the vinyl terminated macromonomer product such as by the processes described in GB 1550419A, U.S. Pat. Nos. 3,647,906 and 3,592,866. Useful fractions include ranges from about 4 carbon-numbers up to 20 carbon-numbers, e.g., C₄-C₈, C₄-C₁₄, C₄-C₂₀. The lower α -olefin fraction may contain α -olefins having the same carbon-number as the lowest α -olefin in the higher α -olefin fraction, but preferably contains only α -olefins of carbon-numbers lower than the carbon-number of the lowest α -olefin in the higher α -olefin fraction. The higher α -olefin fraction may include α -olefins of the same carbon number as the highest α -olefin in the lower α -olefin fraction up to the highest α -olefin produced in the reaction, but generally not higher than C₄₀. Preferably, however, the higher α -olefin fraction contains only α -olefins of carbon-numbers higher than the carbon number of the highest α -olefin in the lower α -olefin fraction.

In a separation where an α -olefin product mixture free of light oligomers, e.g., dimers, trimers, tetramers, etc., is desired, the lower α -olefin fraction is further separated into a light α -olefin fraction and an intermediate α -olefin fraction. The light α -olefin fraction may include from C₄ up to C₁₂, e.g., C₄-C₆, C₄-C₈, C₄-C₁₀, etc. In this modification, the inter-

mediate α -olefin fraction is removed as product and the light α -olefin fraction is converted to additional intermediate α -olefins.

In another embodiment, any vinyl terminated macromonomer described herein can be separated into different boiling point cuts by distillation performed according to the procedures described in ASTM methods D2892 and D5236. (D2892: Standard Test Method for Distillation of Crude Petroleum (15-Theoretical Plate Column) and D5236: Standard Test Method for Distillation of Heavy Hydrocarbon Mixtures (Vacuum Potstill Method).)

For example, a low molecular weight atactic polypropylene VTM (677.3 gram charge) can be fractionated or distilled using the boiling point range, mass recovery, vacuum conditions listed below. Both initial boiling point (IBP) and final boiling point (FBP) are in degree Fahrenheit (° F.) and corrected to atmospheric pressure.

Fraction (Cut) #	Initial boiling point/IBP (° F.)	Final boiling point/FBP (° F.)	Weight of collected fraction (grams)	Still pressure (mmHg)	ASTM method used
Charge (Feed)	—	—	677.3		
1	IBP	140	3.8	760	D2892
2	140	160	11.9	760	D2892
3	160	265	27.8	760	D2892
4	265	365	35.0	88	D2892
5	365	465	46.6	88	D2892
6	465	525	34.4	88	D2892
7	525	568	44.0	10	D2892
8	568	588	14.2	10	D2892
9	588	645	53.1	10	D2892
10	645	700	63.4	2	D2892
11	700	844	41.2	0.2	D5236
12	844	892	42.3	0.2	D5236
13	892	904	17.9	0.2	D5236
Distillation Bottoms	904+	—	226.6	—	—

As shown in the table above, total recovery of collected fractions (fraction 1 to 13) with boiling points between 25° C. and 904° F. was 435.6 g (64.3 wt % of initial charge). Total recovery of distillation bottoms with boiling point above 904° F. was 226.6 g (33.5 wt % of initial charge). The total recovery of both distilled fractions and bottoms material amounts to 97.8 wt %. The resulting distilled fractions and distillation bottoms have narrow molecular weight distributions (Mw/Mn <1.4) as determined by GPC.

In any embodiment described herein, the vinyl terminated macromonomer (preferably comprising propylene, preferably at least 50 mol % propylene, preferably at least 70 mol %, propylene, preferably at least 85 mol %, preferably at least 90 mol %, preferably at least 95 mol %, preferably 100 mol % propylene) has a % m diads (where % m + % r diads = 100) determined by ¹³C nuclear magnetic resonance (NMR) ranging from 70 to 20, preferably from 60 to 30, more preferably from 55 to 40. % m diads and % r diads are discussed in L. Resconi, L. Cavallo, A. Fait, and F. Piemontesi, *Chem. Rev.* 2000, 100, pp. 1253-1345, as well as H. N. Cheng, *Macromolecules*, 17, p. 1950 (1984).

In another embodiment of the invention, the vinyl terminated macromonomer (preferably a propylene based vinyl terminated macromonomer, preferably a homopolypropylene vinyl terminated macromonomer) has less than 1 mol % regio defects (as determined by ¹³C NMR), based upon the total propylene monomer. Three types of defects are defined to be the regio defects: 2,1-erythro, 2,1-threo, and 3,1-isomerization. The structures and peak assignments for these are

given in L. Resconi, L. Cavallo, A. Fait, and F. Piemontesi, *Chem. Rev.* 2000, 100, pp. 1253-1345, as well as H. N. Cheng, *Macromolecules*, 17, p. 1950 (1984). Alternately, the vinyl terminated macromonomer (preferably a propylene based vinyl terminated macromer, preferably a homopolypropylene vinyl terminated macromonomer) has less than 250 regio defects per 10,000 monomer units (as determined by ^{13}C NMR), preferably less than 150, preferably less than 100, preferably less than 50 regio defects per 10,000 monomer units. The regio defects each give rise to multiple peaks in the carbon NMR spectrum, and these are all integrated and averaged (to the extent that they are resolved from other peaks in the spectrum), to improve the measurement accuracy. The chemical shift offsets of the resolvable resonances used in the analysis are tabulated below. The precise peak positions may shift as a function of NMR solvent choice.

Regio defect	Chemical shift range (ppm)
2,1-erythro	42.3, 38.6, 36.0, 35.9, 31.5, 30.6, 17.6, 17.2
2,1-threo	43.4, 38.9, 35.6, 34.7, 32.5, 31.2, 15.4, 15.0
3,1 insertion	37.6, 30.9, 27.7

The average integral for each defect is divided by the integral for one of the main propylene signals (CH_3 , CH , CH_2), and multiplied by 10000 to determine the defect concentration per 10,000 monomers.

In another embodiment, any vinyl terminated macromonomer described herein may have a melting point (DSC first melt) of from 60° C. to 160° C., alternately 50° C. to 145° C., alternately 50° C. to 130° C., alternately 50° C. to 100° C. In another embodiment, the vinyl terminated macromonomer described herein have no detectable melting point by DSC following storage at ambient temperature (23° C.) for at least 48 hours.

In another embodiment, the vinyl terminated macromonomer described herein may have a glass transition temperature of less than 0° C. or less (DSC), preferably -10° C. or less, more preferably -20° C. or less, more preferably -30° C. or less, more preferably -50° C. or less.

Melting temperature (T_m) and glass transition temperature (T_g) are measured using Differential Scanning calorimetry (DSC) using commercially available equipment such as a TA Instruments 2920 DSC. Typically, 3 to 10 mg of the sample, that has been stored at 25° C. for at least 48 hours, is sealed in an aluminum pan, and loaded into the instrument at 25° C. The sample is equilibrated at 25° C., then it is cooled at a cooling rate of 10° C./min to -80° C. The sample is held at -80° C. for 5 min and then heated at a heating rate of 10° C./min to 25° C. The glass transition temperature is measured from the heating cycle. Alternatively, the sample is equilibrated at 25° C., then heated at a heating rate of 10° C./min to 150° C. The endothermic melting transition, if present, is analyzed for onset of transition and peak temperature. The melting temperatures reported are the peak melting temperatures from the first heat unless otherwise specified. For samples displaying multiple peaks, the melting point (or melting temperature) is defined to be the peak melting temperature (i.e., associated with the largest endothermic calorimetric response in that range of temperatures) from the DSC melting trace.

In another embodiment, the vinyl terminated macromonomers described herein are a liquid at 25° C.

In a particularly preferred embodiment of the invention, the vinyl terminated macromonomer (preferably comprising pro-

pylene, at least 50 mol % propylene, preferably at least 70 mol % propylene) has less than 250 regio defects per 10,000 monomer units, preferably less than 150, preferably less than 100, preferably less than 50 regio defects per 10,000 monomer units, and a T_g of less than 0° C. or less (DSC), preferably -10° C. or less, more preferably -20° C. or less, more preferably -30° C. or less, more preferably -50° C. or less.

In another embodiment, the vinyl terminated macromonomers described herein have a viscosity at 60° C. of greater than 1000 cP, greater than 12,000 cP, or greater than 100,000 cP. In other embodiments, the vinyl terminated macromonomer have a viscosity of less than 200,000 cP, less than 150,000 cP, or less than 100,000 cP. Viscosity is defined as resistance to flow and the melt viscosity of neat copolymers is measured at elevated temperature using a Brookfield Digital Viscometer.

In another embodiment, the VTM described herein also has a viscosity (also referred to a Brookfield Viscosity or Melt Viscosity) of 90,000 mPa-sec or less at 190° C. (as measured by ASTM D 3236 at 190° C.; ASTM=American Society for Testing and Materials); or 80,000 mPa-sec or less, or 70,000 mPa-sec or less, or 60,000 mPa-sec or less, or 50,000 mPa-sec or less, or 40,000 mPa-sec or less, or 30,000 mPa-sec or less, or 20,000 mPa-sec or less, or 10,000 mPa-sec or less, or 8,000 mPa-sec or less, or 5000 mPa-sec or less, or 4000 mPa-sec or less, or 3000 mPa-sec or less, or 1500 mPa-sec or less, or between 250 and 6000 mPa-sec, or between 500 and 5500 mPa-sec, or between 500 and 3000 mPa-sec, or between 500 and 1500 mPa-sec; and/or a viscosity of 8,000 mPa-sec or less at 160° C. (as measured by ASTM D 3236 at 160° C.), or 7,000 mPa-sec or less, or 6,000 mPa-sec or less, or 5,000 mPa-sec or less, or 4,000 mPa-sec or less, or 3,000 mPa-sec or less, or 1,500 mPa-sec or less, or between 250 and 6000 mPa-sec, or between 500 and 5500 mPa-sec, or between 500 and 3000 mPa-sec, or between 500 and 1500 mPa-sec. In other embodiments, the viscosity is 200,000 mPa-sec or less at 190° C., depending on the application. In other embodiments, the viscosity is 50,000 mPa-sec or less, depending on the applications.

Other suitable macromonomers useful in the present invention include those disclosed in U.S. Pat. Nos. 7,795,347 and 6,169,154, the contents of which are incorporated herein in their entirety for all purposes. In addition, a phenoxyimine-based catalyst (FI catalyst) or a pyrroleimine-based catalyst (PI catalyst) can be used to prepare the macromonomers. These catalysts comprise (a) a transition metal compound having phenoxyimine or pyrroleimine as a ligand, and (b) one or more kind(s) of compound selected from (b-1) an organic metal compound, (b-2) an organic aluminumoxy compound, and (b-3) a compound that reacts with the transition metal compound (a) to form an ion pair, as described in JP-A-2001-72706, JP-A-2002-332312, JP-A-2003-313247, JP-A-2004-107486, and JP-A-2004-107563 or as in column 16, line 56 et seq. of U.S. Pat. No. 7,795,347 Formula (XI). Herein, as the transition metal contained in the transition metal compound, the transition metal of Groups 3 to 11 in the periodic table can be used.

Process to Functionalize Polyolefins—Hydroformylation

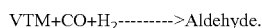
The vinyl terminated macromonomers described herein are preferably subjected to a hydroformylation reaction, also referred to as an OXO reaction or process, such as those processes described U.S. Pat. Nos. 7,345,212; 7,186,874; 7,148,388; 7,081,554; 7,081,553; 6,982,295; 6,969,736; 6,969,735; 6,013,851; 5,877,358; and PCT publications WO2007106215; WO2007040812; WO2006086067; WO2006055106; WO 2005/05878; WO2003050070; WO2000015190. Typically, the hydroformylation produces

aldehydes which may be hydrogenated to the alcohol and subsequently oxidized to the desired acid(s), or directly oxidized to the desired acid(s). The hydroformylation process may generally be carried out in a manner known by the persons skilled in the art, for example by the process according to U.S. Pat. Nos. 4,247,486; 4,287,370; 5,053,551; 6,100,432; WO 02/00582, and DE 10128325, although with some of them, higher temperatures and/or longer residence times and/or carbon monoxide partial pressures will be used.

Hydroformylation is a process in which an olefin, such as a vinyl terminated macromonomer, is reacted with carbon monoxide and hydrogen in the presence of a catalyst to form aldehydes and alcohols typically containing one carbon atom more than the feed olefin. There are two principal technology families used in commercial hydroformylation processes. One is known as the low or medium pressure oxo process family and generally involves the use of a catalyst of an organometallic complex of rhodium with organophosphorous ligands for providing the necessary stability at the lower pressures and operates at pressures from 10 to 50 Bar. The second process family is known as the high or medium-pressure process family and generally involves the use of a cobalt or rhodium based catalyst and typically operates at pressures from 50 to 350 Bar.

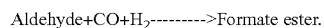
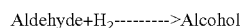
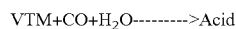
High and medium pressure hydroformylation reactions involve the reaction of liquid materials with normally gaseous materials which are at least partly dissolved in the liquid during reaction due to the high pressure conditions, and gaseous materials may also be entrained as droplets or bubbles in the liquid phase. Unreacted materials are vented off after the reaction. The starting liquids that are involved in high pressure hydroformylation comprise olefins, i.e., vinyl terminated macromonomers, may be mixtures of olefins and/or vinyl terminated macromonomers. The gases that are involved in high and medium pressure hydroformylation include carbon monoxide and hydrogen, frequently supplied in a mixture that is known as synthesis gas or "syngas." Syngas can be obtained through the use of partial oxidation technology (POX), or steam reforming (SR), or a combination thereof that is often referred to as autothermal reforming (ATR). It can be generated from almost every carbon containing source material, including methane, natural gas, ethane, petroleum condensates like propane and/or butane, naphtha or other light boiling hydrocarbon liquids, gasoline, or distillate-like petroleum liquids, but also including heavier oils and byproducts from various processes including hydroformylation, and even from coal and other solid materials like biomass and waste plastics. The gaseous feed streams can also contain inert components such as nitrogen, helium, argon, methane, and carbon dioxide which, although mostly inert, can be significant in that they have a dilution effect and can help to control reaction temperature. Nitrogen, helium, and argon can come in as impurities with the oxygen supply, or when air or enriched air is used as feed for syngas generation.

The main hydroformylation reaction is the reaction of a vinyl terminated macromonomer with carbon monoxide and hydrogen to produce an aldehyde,

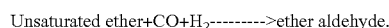
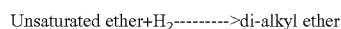


This reaction typically consumes equimolar amounts of CO and H₂. Its rate of reaction is proportional to the ratio of hydrogen-to-CO. When the fresh feed syngas does not contain CO and hydrogen in equal molar amounts, this H₂/CO ratio is bound to change as the reaction progresses through the hydroformylation reactor zone. Also, there are a number of

competing and consecutive gas consuming reactions in which the CO and H₂ is not necessarily consumed in an equimolar ratio, for example:



Aldehydes can condense with alcohols to form a hemiacetal, R₁—CHOH—O—R₂, which is not very stable and splits off water to form an unsaturated ether. This again can undergo gas consuming reactions:



All these other gas consuming reactions also affect the quantity of CO and hydrogen present throughout each reactor and throughout the series of reactors.

In an industrial hydroformylation plant that is producing alcohols, at least part of the product of hydroformylation, which consists primarily of aldehydes, or of mixtures of alcohols, aldehydes and formate esters, potentially together with various other compounds, is hydrogenated to convert the aldehydes and formate esters to alcohols and/or to reduce the level of the impurities. On certain catalysts, these formate esters can, amongst others, split into an alcohol and carbon monoxide, which, in the presence of water, can undergo the water-gas-shift reaction and produce hydrogen and carbon dioxide. Alternatively, the formate ester can hydrolyse with water to form the alcohol and formic acid, which then can decompose into carbon monoxide and hydrogen. This formed hydrogen is then available to participate in the hydrogenation reaction. Overall, the hydrogenation reaction is typically operated with a stoichiometric excess of hydrogen, and can therefore result in a stream of unreacted hydrogen.

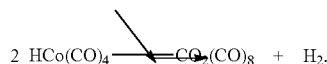
The products of hydroformylation, predominantly aldehydes and alcohols, but also some formate esters and possibly including heavy materials, are typically fed at least partially, as such, or optionally, after distillation, to a hydrogenation reactor. This is usually done after catalyst removal and the products are then hydrogenated to produce alcohols. There is generally an excess of hydrogen in the hydrogenation reactor, which is left over as a waste stream. Optionally, a part of the aldehydes from the hydroformylation reaction may be separated off for use as such or for being converted into carboxylic acids.

Hydroformylation processes are typically performed at elevated temperature and pressure in the presence of a hydroformylation catalyst. The optimum temperature and pressure often depends upon the nature of the feed both in terms of the carbon number(s) of the VTM, the structure of the VTM (linear or branched structure) and the concentration of the VTM in the feed. The feed is typically a mixture of saturated and unsaturated (predominantly unsaturated) materials. Typical pressures are from 50 to 350 bar, preferably 150 or 250 to 350 bar, most preferably from 275 to 325 bar. Typical temperatures range from 120° C. to 185° C. or 190° C., preferably from 165° C. or 170° C. to 180° C. or 185° C., although many feeds may preferably be hydroformylated at lower temperatures such as from 100° C. or 120° C. to 140° C. for reasons of reactivity or reaction selectivity. The catalyst used in the high pressure hydroformylation is typically either a rhodium or a cobalt catalyst. Preferably, the active cobalt catalyst is hydrocobaltcarbonyl and the rhodium catalyst comprises

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rhodiumcarbonyls. When using cobalt, typical cobalt concentrations of up to 0.8 wt % cobalt on the VTM content of the feed may be used, preferably from 0.02 wt % or 0.05 wt % to 0.8 wt % cobalt, more preferably from 0.1 wt % to 0.5 wt %. When using rhodium, much lower concentrations may be used, such as 0.1 to 200 ppm by weight relative to the VTM feed, preferably 0.2 to 50 ppm, more preferably 0.3 to 20 ppm, even more preferably 0.4 to 5 ppm by weight.

The catalyst may be supplied already absorbed in the feed and/or as fresh catalyst. In the case of cobalt, the initial cobalt species may be dicobalt octacarbonyl $\text{Co}_2(\text{CO})_8$ or a salt of cobalt with an acid, e.g., cobalt carbonate or a salt of cobalt with another acid of moderate strength and preferably with an organic acid. Such organic salts may, for example, be with formic acid or acetic acid, or with higher molecular weight acids like oleic, stearic, or naphthenic acids, or with the heavier carboxylic acids that are made as byproducts in the hydroformylation step or its downstream catalyst removal step and that survive the hydrogenation treatment, eventually ending up in the heavy oxonation fraction byproduct of the aldehyde or alcohol distillation step. The catalyst may also be cobalt oxide or hydroxide. This cobalt source may be performed in a separate reactor in order to convert it to the carbonyl form, or this conversion may occur in the hydroformylation reactor itself. Under the hydroformylation conditions, an equilibrium is believed to establish itself between two cobaltcarbonyls:



Hydr(id)ocobalt(tetra)carbonyl ($\text{HCo}(\text{CO})_4$) is generally believed to be the active catalyst form, or at least the precursor to the active catalyst form, which also may be $\text{HCo}(\text{CO})_3$. The higher the hydrogen partial pressure in the hydroformylation reaction and the higher the temperature, the greater the concentration of hydrocobalt carbonyl, and hence the greater the reaction rate.

Where cobalt catalyzed hydroformylation is used, the product is decobalted. In one embodiment, this is done by neutralizing the active cobalt species $\text{HCo}(\text{CO})_4$, with a base such as sodium hydroxide or carbonate in a decobalder. The decobalder conditions are such that the neutralization converts the hydrocobalt carbonyl to sodium cobalt carbonyl. Preferred conditions are to use a stoichiometric excess of sodium hydroxide or carbonate above the amount needed for cobalt neutralization, an excess of 100% to 200%, particularly 140% to 180% is useful. The decobalder is typically operated at a temperature in the range 155° C. to 165° C. and it is preferred that sufficient carbon dioxide and/or carbonate is present in the decobalder to ensure the formation of sodium cobalt carbonyl and to also buffer the pH in the range 7.8 to 8.5. This technique is described in more detail in WO 2006/122526.

Alternative embodiments use techniques for the decobalting of the product of cobalt catalyzed hydroformylation by oxidative methods, and are described in WO 2008/128852, which are conveniently used together with the techniques of the present invention. Yet, other suitable techniques are described in U.S. Pat. Nos. 5,237,105; 5,218,134; and 4,625,067; 8,476,476; and 8,541,627.

The hydroformylation reaction is exothermic and the reaction is typically fast. The quantity of heat given off and the rate of heat release to some extent depend upon the nature and structure of the VTM that is being subject to hydroformylation. In the case of cobalt catalyst, the ratio of hydrogen to

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carbon monoxide in the fresh syngas is typically about 1.3:1, since at this ratio the plating out of the cobalt is substantially avoided, or sufficiently low to be acceptable.

Hydroformylation reactors useful in the present invention are continuous reactors which are preferably gas-lift reactors like those described in U.S. Pat. Nos. 3,830,846; 4,320,237; PCT publication WO 01/14297; GB 1,308,206, and, more preferably, are loop reactors such as those described in U.S. Pat. Nos. 4,312,837; 4,379,124; or PCT publication WO 97/29018.

After passing through one, or a series of reactors, the final product of the hydroformylation reaction comprises a mixture of alcohols, aldehydes, unreacted VTMs, paraffins, formate esters, and heavy oxo fraction, comprising dimer and higher condensation products such as ethers, esters, acetals, hemi-acetals, ether aldehydes, ether alcohols, etc., hydrogen, carbon monoxide, generally catalyst residues, and inert materials. The product is often purified and separated into its components.

The purification involves, amongst other steps, the removal of dissolved and entrained catalyst species which may be recycled for further use. For cobalt catalyzed reactions, the first step in the purification may be the removal of cobalt at high pressure, and the preferred method is by injection of optionally hot and dilute caustic soda and/or sodium carbonate into the reaction product in a decobalder vessel following the final hydroformylation reactor. In the decobalder the majority of the cobalt is converted into $\text{NaCo}(\text{CO})_4$, the water soluble sodium salt of hydrocobaltcarbonyl. If sodium carbonate is used or carbon dioxide is present, a small portion of the cobalt may be converted into solid cobalt carbonate. In absence of carbon dioxide or sodium carbonate, cobalt may be converted to solid cobalt hydroxide, $\text{Co}(\text{OH})_2$. The decobalder conditions are such that the neutralization converts the hydrocobalt carbonyl to sodium cobalt carbonyl. In this way, the presence of cobalt in the waste water can be avoided. Preferred conditions are to use a stoichiometric excess of sodium hydroxide or carbonate above the amount needed for cobalt neutralization, an excess of 30% to 200%, e.g., 100% to 200%, particularly 50% or 100% or 140% to 180% is useful. The decobalder is typically operated at a temperature in the range 125° C. or 140° C. to 170° C., preferably 155° C. to 165° C. It is preferred that sufficient carbon dioxide and/or carbonate is present in the decobalder to buffer the pH of the water separating downstream in the range 7.8 to 8.5. Further possible embodiments can be found in U.S. Pat. No. 5,130,107.

Alternative to this alkaline decobalting method at high pressures, the cobalt may be removed by an acidic and/or oxidative method as described in J. Falbe in WO 01/14297, also in U.S. Pat. Nos. 4,625,067; 5,130,107; 5,235,112; 5,237,104; 5,237,105; 5,321,168; 5,354,908; 5,410,090; 5,457,240; also FR 1089983; EP 642488; EP 643683; PCT publications WO 03/082788; and WO 03/082789.

The hydroformylation product, optionally decobalted and combined with the separate water phase formed during decobalting, comprises dissolved gas, entrained gas, water, and the hydroformylation product itself. It may be fed, possibly after cooling, to a high pressure separator which separates the free gas from the liquid phase as high pressure offgas. Typically, the high pressure separator operates at a pressure of 250 bar or higher. The preferred pressure is in the range 250 to 300 bar with 260 to 270 bar being most preferred. The gas is separated off and the amount required for recycle is sent to an offgas recycle compressor system. Any excess gas may be disposed of. Such purge may be used to control the recycle gas composition. In addition, unwanted gases such as excess

nitrogen and other non-condensables may also, at least partially, be removed to ensure that the recycle of gases, according to the present invention, does not result in an undesirable build up of inert gases such as nitrogen in the hydroformylation reactors.

As a general guide the pressure at the end of the hydroformylation reaction is kept above 170 bar, preferably above 190 or 200 bar, more preferably above 210 or 220 bar, most preferably above 240 bar, in order to avoid cobalt plating in the hydroformylation reactors. The carbon monoxide content of the offgas from the high pressure separator is desirably such that the partial pressure of CO is above 75 bar, preferably above 77 bar, preferably above 84 bar, since if the partial pressure drops below these levels, cobalt plating can occur in the hydroformylation reactors. Similarly, the hydrogen content of the offgas from the high pressure separator should be such that the partial pressure of hydrogen is desirably above 75 bar, preferably above 77 bar, preferably above 84, more preferably above 91 bar, since if the partial pressure drops below this level there is a drop in reaction rate.

Another important aspect of the hydroformylation reaction is the reaction temperature and temperature control. The reaction is highly exothermic and the temperature generated depends on the reactivity of the VTMs and the concentration and ratio of the reactive materials, the catalyst concentration, and the volume of inert material present. Accordingly, the recycle gases can be used to adjust the amounts and ratios of the reactive materials present and the composition of the recycle gases can be adjusted as a component of reaction temperature control. The reactors are also provided with cooling systems. These can be internal cooling coils or piping, or a jacket around the reactor, or a heat exchanger that is made part of the reactor, as disclosed in WO 01/29018, or a combination thereof.

In order to improve the selectivity of the hydroformylation reaction, water may be injected into the hydroformylation reactors. We have found that the injection of water reduces the formation of formate esters and heavy by-products. When used, water should be injected into the first reactor and may also be injected into any second and subsequent reactors that are used, but we have found that this is not always essential.

In a particularly preferred embodiment, this invention further relates to a process to functionalize polyolefins, both polymers and oligomers, comprising contacting a catalyst, typically a Rh or cobalt catalyst, and one or more vinyl terminated macromonomers in the presence of carbon monoxide and, optionally, hydrogen. The reactants are typically combined in a reaction vessel at a temperature of -50°C . to 300°C . (preferably 25°C . to 150°C .). Likewise, the reactants are typically combined at a pressure of 0 to 1000 MPa (preferably 0.5 to 500 MPa, preferably 1 to 250 MPa) for a residence time of 0.5 seconds to 10 hours (preferably 1 second to 5 hours, preferably 1 minute to 1 hour). In some embodiments, from about 50 psi up to the pressure permitted by the reactor, e.g., 3,000 psi, is utilized for the reactants.

Typically, 1×10^{-1} to 1×10^{-6} moles, preferably 1×10^{-2} to 1×10^{-5} moles, preferably 1×10^{-3} to 1×10^{-4} moles of catalyst are charged to the reactor per mole of VTM charged.

Typically, a ratio of carbon monoxide to hydrogen of 1 to 1.1 moles, preferably 1 to 1.2 moles, preferably 1 to 2 moles, are charged to the reactor.

Total psi of CO/H_2 and solvent is preferably about 200 psi.

The process is typically a solution process, although it may be a bulk or high pressure process. Homogeneous processes are preferred. (A homogeneous process is defined to be a process where at least 90 wt % of the product is soluble in the reaction media.) A bulk homogeneous process is particularly

preferred. (A bulk process is defined to be a process where reactant concentration in all feeds to the reactor is 70 vol % or more.) Alternately, no solvent or diluent is present or added in the reaction medium (except for the small amounts used as the carrier for the catalyst or other additives, or amounts typically found with the reactants; e.g., propane in propylene).

Suitable diluents/solvents for the process include non-coordinating, inert liquids. Examples include straight and branched-chain hydrocarbons such as isobutane, butane, pentane, isopentane, hexanes, isohexane, heptane, octane, dodecane, and mixtures thereof; cyclic and alicyclic hydrocarbons such as cyclohexane, cycloheptane, methylcyclohexane, methylcycloheptane, and mixtures thereof such as can be found commercially (IsoparTM); and perhalogenated hydrocarbons such as perfluorinated C_{4-10} alkanes, chlorobenzene, and aromatic and alkylsubstituted aromatic compounds such as benzene, toluene, mesitylene, and xylene. In a preferred embodiment, the feed concentration for the process is 60 vol % solvent or less, preferably 40 vol % or less, preferably 20 vol % or less.

The process may be batch, semi-batch, or continuous. As used herein, the term continuous means a system that operates without interruption or cessation. For example, a continuous process to produce a polymer would be one where the reactants are continually introduced into one or more reactors and polymer product is continually withdrawn.

Useful reaction vessels include reactors, including continuous stirred tank reactors, batch reactors, reactive extruder, pipe, or pump.

This invention further relates to a process, preferably an in-line process, preferably a continuous process, to produce functionalized polyolefins, comprising introducing macromonomer, carbon monoxide/hydrogen, and catalyst system into a reactor, obtaining a reactor effluent containing aldehyde terminated polyolefin, optionally removing (such as flashing off) solvent, unused monomer and/or other volatiles, obtaining aldehyde terminated polyolefin (such as those described herein), preferably an in-line process, preferably a continuous process, to produce functionalized polyolefins, comprising introducing vinyl terminated polyolefin, catalyst (as described herein) and carbon monoxide/hydrogen (as described herein) into a reaction zone (such as a reactor, an extruder, a pipe, and/or a pump), and obtaining functionalized polyolefin (such as those described herein).

Aldehydes are synthesized by the hydroformylation of vinyl terminated macromonomers in high yield and purity. Common transition metal complexes useful for hydroformylation often employ Rh, Co, and other metals. A particularly useful catalyst is $\text{Rh}(\text{Acac})_3$ with added $\text{P}(\text{Ph})_3$ to yield about 90% 1-aldehyde with the remainder being 2-aldehydes and some alcohol by-product. The alcohol does not interfere with these reactions. The aldehydes used in the present invention may also be produced by other methods and are not limited to the hydroformylation procedure.

Catalysts

The hydroformylation reaction, also known as the oxo reaction, is used extensively in commercial processes for the preparation of aldehydes typically by the reaction of one mole of an olefin with one mole each of hydrogen and carbon monoxide. A catalyst system containing a Group VIII metal, such as rhodium or cobalt, is used to catalyze the oxo process. In addition, a phosphorus ligand such as halophosphites, phosphites, and phosphines can be used to regulate the activity of the Group VIII metal. Hydroformylation catalysts are known by those having ordinary skill in the art and include, for example, $\text{HCo}(\text{CO})_3$, $\text{HRh}(\text{CO})(\text{PPh}_3)_2$, and those described in Catal. Sci. Technol., 2012, 2, pp. 773-777. Typi-

cally, the ligand tributylphosphine (PBu_3) is added to the reaction mixture to help improve yields. In a preferred embodiment, the amounts of Rh precursor added are in the range noted above and PPh_3/Rh is about 7/1.

Rhodium catalysts are useful herein, such as those described in EP 0 804 400. Rhodium catalysts containing an organophosphorus ligand are particularly useful. Hydroformylation reactions have generally employed rhodium catalyst stabilized by phosphorus containing ligands operated in what is known as the low pressure oxo (LPO) technology originally developed by Union Carbide Corporation and licensed from Davy Process Technology. In another hydroformylation technology, cobalt containing catalysts are used and the process is operated at higher pressures. In a similar way to cobalt, also rhodium catalyzed hydroformylation may be operated at higher pressures, without a stabilizing ligand other than carbon monoxide or with a weak ligand like, e.g., triphenylphosphine oxide (TPPO).

The hydroformylation is preferably carried out in the presence of a catalyst comprising a rhodium complex in conjunction with an organophosphorus ligand. This organophosphorus ligand may be a tertiary organophosphine or an organophosphite. The process employing triphenylphosphine (TPP) or other phosphines is typically operated at conditions of high phosphorus to rhodium ratio (P/Rh) and low partial pressure of carbon monoxide (p_{CO}). The triorganophosphine ligand can be, for example, a trialkylphosphine such as tributylphosphine, a $\text{C}_1\text{-C}_6$ alkyl diarylphosphine such as butyldiphenylphosphine, an aryl dialkylphosphine such as phenyldibutylphosphine, an aryl dialkyl diphosphine such as cyclohexyldiphenyl phosphine, tetraphenyldiphosphinomethane, 1,2-bis(diphenyl phosphino) ethane, 1,3-bis(diphenyl phosphino) propane, 1,4-bis(diphenyl phosphino) butane, and the bisphosphine ligands described in EP-A 279 018, EP-A 311 619, WO 90/06810, and EP-A 71 281. However, particular phosphines such as triphenylphosphine, tri-*p*-tolylphosphine, trinaphthylphosphine, phenyldinaphthylphosphine, diphenylnaphthylphosphine, tri(*p*-methoxyphenyl)phosphine, tri(*p*-cyanophenyl)phosphine, tri(*p*-nitrophenyl)phosphine, *p*-N,N-dimethylaminophenylbisphenylphosphine, and the like are preferred. Triphenylphosphine (TPP) is most preferred.

Organophosphite ligands can be those disclosed in U.S. Pat. Nos. 4,599,206; 4,668,651; 4,737,588; 4,748,261; 4,769,498; 4,774,361; 4,789,753; 4,835,299; 4,871,880; 4,885,401; 5,179,055; 5,288,918; 5,312,996; 5,364,950; 5,681,473; 5,756,855; and PCT publication WO 97/20793. Preferred is 6,6'-[[3,3',5,5'-tetrakis(1,1-dimethylethyl)-1,1'-biphenyl]-2,2'-diyl]bis(oxy)]bis-dibenzo[d,f][1,3,2]-dioxaphosphin, or 6,6'-[[3,3',5,5'-tetrakis(1,1-dimethylpropyl)-1,1'-biphenyl]-2,2'-diyl]bis(oxy)]bis-dibenzo[d,f][1,3,2]-dioxaphosphin, or 6,6'-[[3,3',5,5'-tetrakis(1,1-dimethylethyl)-5,5'-dimethoxy[1,1'-biphenyl]-2,2'-diyl]bis(oxy)]bis-dibenzo[d,f][1,3,2]-dioxaphosphin, or tris(2,4,6-di-*t*-butylphenyl)-phosphite. Most preferred is 6,6'-[[3,3',5,5'-tetrakis(1,1-dimethylethyl)-1,1'-biphenyl]-2,2'-diyl]bis(oxy)]bis-dibenzo[d,f][1,3,2]-dioxaphosphin. Ionic varieties of such phosphites are disclosed in U.S. Pat. Nos. 5,059,710 and 5,113,022.

In another embodiment of the invention, the catalyst may be a cobalt catalyst, preferably as described in GB 702,242; U.S. Pat. Nos. 4,404,119; 4,419,195; 6,960,699; 7,154,012; 8,017,811; and 7,586,017.

In a particularly useful embodiment, the cobalt catalyst is an organophosphine modified cobalt hydroformylation catalyst, typically comprising cobalt in complex combination with carbon monoxide and an organophosphine ligand. By the term "complex combination" as used herein, is meant a

coordination compound formed by the union of one or more carbon monoxide and organophosphine molecules with one or more cobalt atoms. In its active form, the suitable organophosphine modified cobalt hydroformylation catalyst contains one or more cobalt components in a reduced valence state.

Suitable organophosphine ligands include those having a trivalent phosphorus atom having one available or unshared pair of electrons. Any essentially organic derivative of trivalent phosphorus with the foregoing electronic configuration is a suitable ligand for the cobalt catalyst.

Organic radicals of any size and composition may be bonded to the phosphorus atom. For example, the organophosphine ligand may comprise a trivalent phosphorus having aliphatic and/or cycloaliphatic and/or heterocyclic and/or aromatic radicals satisfying its three valencies. These radicals may contain a functional group such as carbonyl, carboxyl, nitro, amino, hydroxy, saturated and/or unsaturated carbon-to-carbon linkages, and saturated and/or unsaturated non-carbon-to-carbon linkages.

It is also suitable for an organic radical to satisfy more than one of the valencies of the phosphorus atom, thereby forming a heterocyclic compound with a trivalent phosphorus atom. For example, an alkylene radical may satisfy two phosphorus valencies with its two open valencies and thereby form a cyclic compound. Another example would be an alkylene dioxy radical that forms a cyclic compound where the two oxygen atoms link an alkylene radical to the phosphorus atom. In these two examples, the third phosphorus valency may be satisfied by any other organic radical.

Another type of structure involving trivalent phosphorus having an available pair of electrons is one containing a plurality of such phosphorus atoms linked by organic radicals. This type of a compound is typically called a bidentate ligand when two such phosphorus atoms are present, a tridentate ligand when three such phosphorus atoms are present, and so forth.

Suitable organophosphine modified cobalt hydroformylation catalysts for use in the process of the present invention and their methods of preparation are disclosed in U.S. Pat. Nos. 3,369,050; 3,501,515; 3,448,158; 3,448,157; 3,420,898; and 3,440,291, all of which are incorporated herein by reference. Preferably, the organophosphine modified cobalt hydroformylation catalyst is substantially homogeneous with the reaction mixture.

Preferred organophosphine modified cobalt hydroformylation catalysts for use in the process of the present invention are those which include an organic tertiary phosphine ligand, especially a bicyclic heterocyclic tert-phosphine ligand, preferably as disclosed in U.S. Pat. No. 3,501,515. Representative examples of such ligands include: 9-hydrocarbyl-9-phosphabicyclo[4.2.1]nonane; 9-aryl-9-phosphabicyclo[4.2.1]nonane, such as 9-phenyl-9-phosphabicyclo[4.2.1]nonane; (di)alkyl-9-aryl-9-phosphabicyclo[4.2.1]nonane, such as 3,7-dimethyl-9-phenyl-9-phosphabicyclo[4.2.1]nonane, and 3,8-dimethyl-9-phenyl-9-phosphabicyclo[4.2.1]nonane; 9-alkyl-9-phosphabicyclo[4.2.1]nonane, such as 9-octadecyl-9-phosphabicyclo[4.2.1]nonane, 9-hexyl-9-phosphabicyclo[4.2.1]nonane, 9-eicosyl-9-phosphabicyclo[4.2.1]nonane, and 9-triacontyl-9-phosphabicyclo[4.2.1]nonane; 9-cycloalkyl-9-phosphabicyclo[4.2.1]nonane, such as 9-cyclohexyl-9-phosphabicyclo[4.2.1]nonane and 9-(1-octahydro-pentalyl)-9-phosphabicyclo[4.2.1]nonane; 9-cycloalkenyl-9-phosphabicyclo[4.2.1]nonane, such as 9-cyclooctenyl-9-phosphabicyclo[4.2.1]nonane; 9-hydrocarbyl-9-phosphabicyclo[3.3.1]nonane; 9-aryl-9-phosphabicyclo[3.3.1]nonane, such as 9-phenyl-9-phosphabicyclo

[3.3.1]nonane; di)alkyl-9-aryl-9-phosphabicyclo[3.3.1]nonane, such as 3,7-dimethyl-9-phenyl-9-phosphabicyclo[3.3.1]nonane and 3,8-dimethyl-9-phenyl-9-phosphabicyclo[3.3.1]nonane; 9-alkyl-9-phosphabicyclo[3.3.1]nonane, such as 9-octadecyl-9-phosphabicyclo[3.3.1]nonane, 9-hexyl-9-phosphabicyclo[3.3.1]nonane, 9-eicosyl-9-phosphabicyclo[3.3.1]nonane, and 9-triacontyl-9-phosphabicyclo[3.3.1]nonane; 9-cycloalkyl-9-phosphabicyclo[3.3.1]nonane, such as 9-cyclohexyl-9-phosphabicyclo[3.3.1]nonane and 9-(1-octahydropentyl)-9-phosphabicyclo[3.3.1]nonane; 9-cycloalkenyl-9-phosphabicyclo[3.3.1]nonane, such as 9-cyclooctenyl-9-phosphabicyclo[3.3.1]nonane; and mixtures thereof.

A particularly preferred ligand includes a 9-eicosyl-9-phosphabicyclononane compound. A particularly preferred organophosphine modified cobalt hydroformylation catalyst includes a derivative thereof, believed to be a complex comprising cobalt.

The organophosphine modified cobalt hydroformylation catalysts can be prepared by a diversity of methods well known to those skilled in the art as disclosed in U.S. Pat. Nos. 3,369,050; 3,501,515; 3,448,157; 3,420,898; and 3,440,291. A convenient method is to combine a cobalt salt, organic or inorganic, with the desired phosphine ligand, for example, in liquid phase followed by reduction and carbonylation. Suitable cobalt salts comprise, for example, cobalt carboxylates such as acetates, octanoates, etc., as well as cobalt salts of mineral acids such as chlorides, fluoride, sulfates, sulfonates, etc., as well as mixtures of one or more of these cobalt salts. The valence state of the cobalt may be reduced and the cobalt-containing complex formed by heating the solution in an atmosphere of hydrogen and carbon monoxide. The reduction may be performed prior to the use of the organophosphine modified cobalt hydroformylation catalysts or it may be accomplished in-situ with the hydroformylation process in the hydroformylation environment. Alternatively, the organophosphine modified cobalt hydroformylation catalysts can be prepared from a carbon monoxide complex of cobalt. For example, it is possible to start with dicobalt octacarbonyl and, by mixing this substance with a suitable phosphine ligand, the ligand replaces one or more of the carbon monoxide molecules, producing an organophosphine modified cobalt hydroformylation catalyst the active catalyst compound is typically formed under reaction conditions.

Typically, hydroformylated VTM's may be converted to alcohols by known processes, these alcohols being useful for a variety of applications such as intermediates for detergents or plasticizers. The hydroformylated VTM's may be converted to alcohols by a variety of processes, such as the oxo process followed by hydrogenation, or by a modified, single-step oxo process (the modified Shell process), see for instance B. Elvers, et al., Ed., Ullmann's Encyclopedia of Chemical Technology, 5th Ed., Vol. A18, VCH Verlagsgesellschaft mbH, Weinheim, 1991, pp. 321-327.

Optional Support Materials

In embodiments herein, the catalyst system may comprise an inert support material. Preferably, the supported material is a porous support material, for example, talc, and inorganic oxides. Other support materials include zeolites, clays, organoclays, or any other organic or inorganic support material and the like, or mixtures thereof.

Preferably, the support material is an inorganic oxide in a finely divided form. Suitable inorganic oxide materials for use in catalyst systems herein include Groups 2, 4, 13, and 14 metal oxides, such as silica, alumina, and mixtures thereof. Other inorganic oxides that may be employed either alone or in combination with the silica, or alumina are magnesia,

titania, zirconia, and the like. Other suitable support materials, however, can be employed, for example, finely divided functionalized polyolefins, such as finely divided polyethylene. Particularly useful supports include magnesia, titania, zirconia, montmorillonite, phyllosilicate, zeolites, talc, clays, and the like. Also, combinations of these support materials may be used, for example, silica-chromium, silica-alumina, silica-titania, and the like. Preferred support materials include Al_2O_3 , ZrO_2 , SiO_2 , and combinations thereof, more preferably SiO_2 , Al_2O_3 , or $\text{SiO}_2/\text{Al}_2\text{O}_3$.

It is preferred that the support material, most preferably an inorganic oxide, has a surface area in the range of from about 10 to about 700 m^2/g , pore volume in the range of from about 0.1 to about 4.0 cc/g and average particle size in the range of from about 5 to about 500 μm . More preferably, the surface area of the support material is in the range of from about 50 to about 500 m^2/g , pore volume of from about 0.5 to about 3.5 cc/g and average particle size of from about 10 to about 200 μm . Most preferably, the surface area of the support material is in the range is from about 100 to about 400 m^2/g , pore volume from about 0.8 to about 3.0 cc/g and average particle size is from about 5 to about 100 μm . The average pore size of the support material useful in the invention is in the range of from 10 to 1000 \AA , preferably 50 to about 500 \AA , and most preferably 75 to about 350 \AA . In some embodiments, the support material is a high surface area, amorphous silica (surface area=300 m^2/gm ; pore volume of 1.65 cm^3/gm). Preferred silicas are marketed under the tradenames of DAVISON 952 or DAVISON 955 by the Davison Chemical Division of W. R. Grace and Company. In other embodiments DAVISON 948 is used.

The support material should be dry, that is, free of absorbed water. Drying of the support material can be effected by heating or calcining at about 100° C. to about 1000° C., preferably at least about 600° C. When the support material is silica, it is heated to at least 200° C., preferably about 200° C. to about 850° C., and most preferably at about 600° C.; and for a time of about 1 minute to about 100 hours, from about 12 hours to about 72 hours, or from about 24 hours to about 60 hours. The calcined support material must have at least some reactive hydroxyl (OH) groups to produce supported catalyst systems of this invention. The calcined support material is then contacted with at least one polymerization catalyst comprising at least one metallocene compound and an activator.

The support material, having reactive surface groups, typically hydroxyl groups, is slurried in a non-polar solvent and the resulting slurry is contacted with a solution of a catalyst compound and an activator. In some embodiments, the slurry of the support material is contacted with the catalyst for a period of time in the range of from about 0.5 hours to about 24 hours, from about 2 hours to about 16 hours, or from about 4 hours to about 8 hours.

The mixture of the catalyst, activator and support is heated to about 0° C. to about 70° C., preferably to about 23° C. to about 60° C., preferably at 25° C. Contact times typically range from about 0.5 hours to about 24 hours, from about 2 hours to about 16 hours, or from about 4 hours to about 8 hours.

Suitable non-polar solvents are materials in which all of the reactants used herein are at least partially soluble and which are liquid at reaction temperatures. Preferred non-polar solvents are alkanes, such as isopentane, hexane, n-heptane, octane, nonane, and decane, although a variety of other materials including cycloalkanes, such as cyclohexane, aromatics, such as benzene, toluene, and ethylbenzene, may also be employed.

Blends of Functionalized Polyolefins

In some embodiments, the functionalized (and optionally derivitized) polyolefins produced by this invention may be blended with from 0.5 to 99 wt % (typically 1.0 to wt % to 98 wt %, and ideally about 50 wt % to about 98 wt %) of one or more other polymers, including but not limited to, thermoplastic polymer(s) and/or elastomer(s).

By thermoplastic polymer(s) is meant a polymer that can be melted by heat and then cooled without appreciable change in properties. Thermoplastic polymers typically include, but are not limited to, polyolefins, polyamides, polyesters, polycarbonates, polysulfones, polyacetals, polylactones, acrylonitrile-butadiene-styrene resins, polyphenylene oxide, polyphenylene sulfide, styrene-acrylonitrile resins, styrene maleic anhydride, polyimides, aromatic polyketones, or mixtures of two or more of the above. Preferred polyolefins include, but are not limited to, polymers comprising one or more linear, branched or cyclic C_2 to C_{40} olefins, preferably polymers comprising propylene copolymerized with one or more C_3 to C_{40} olefins, preferably a C_3 to C_{20} alpha-olefin, more preferably C_3 to C_{10} alpha-olefins. More preferred polyolefins include, but are not limited to, polymers comprising ethylene including but not limited to ethylene copolymerized with a C_3 to C_{40} olefin, preferably a C_3 to C_{20} alpha-olefin, more preferably propylene and/or butene.

By elastomers is meant all natural and synthetic rubbers, including those defined in ASTM D1566. Examples of preferred elastomers include, but are not limited to, ethylene propylene rubber, ethylene propylene diene monomer rubber, styrenic block copolymer rubbers (including SI, SIS, SB, SBS, SIBS, and the like, where S=styrene, I=isobutylene, and B=butadiene), butyl rubber, halobutyl rubber, copolymers of isobutylene and para-alkylstyrene, natural rubber, polyisoprene, copolymers of butadiene with acrylonitrile, polychloroprene, alkyl acrylate rubber, chlorinated isoprene rubber, acrylonitrile chlorinated isoprene rubber, polybutadiene rubber (both cis and trans).

In another embodiment, the functionalized (and optionally derivitized) polyolefins produced herein may further be combined with one or more of polybutene, ethylene vinyl acetate, low density polyethylene (density 0.915 to less than 0.935 g/cm³) linear low density polyethylene, ultra low density polyethylene (density 0.86 to less than 0.90 g/cm³), very low density polyethylene (density 0.90 to less than 0.915 g/cm³), medium density polyethylene (density 0.935 to less than 0.945 g/cm³), high density polyethylene (density 0.945 to 0.98 g/cm³), ethylene vinyl acetate, ethylene methyl acrylate, copolymers of acrylic acid, polymethylmethacrylate or any other polymers polymerizable by a high-pressure free radical process, polyvinylchloride, polybutene-1, isotactic polybutene, ABS resins, ethylene-propylene rubber (EPR), vulcanized EPR, EPDM, block copolymer, styrenic block copolymers, polyamides, polycarbonates, PET resins, crosslinked polyethylene, copolymers of ethylene and vinyl alcohol (EVOH), polymers of aromatic monomers such as polystyrene, poly-1 esters, polyacetal, polyvinylidene fluoride, polyethylene glycols and/or polyisobutylene. Preferred polymers include those available from ExxonMobil Chemical Company in Baytown, Tex. under the tradenames EXCEEDTM and EXACTTM.

Tackifiers may be blended with the functionalized (and optionally derivitized) polyolefins produced herein and/or with blends of the functionalized (and optionally derivitized) polyolefins produced by this inventions (as described above). Examples of useful tackifiers include, but are not limited to, aliphatic hydrocarbon resins, aromatic modified aliphatic hydrocarbon resins, hydrogenated polycyclopentadiene resins, polycyclopentadiene resins, gum rosins, gum rosin esters, wood rosins, wood rosin esters, tall oil rosins, tall oil rosin esters, polyterpenes, aromatic modified polyterpenes,

terpene phenolics, aromatic modified hydrogenated polycyclopentadiene resins, hydrogenated aliphatic resin, hydrogenated aliphatic aromatic resins, hydrogenated terpenes and modified terpenes, and hydrogenated rosin esters. In some embodiments the tackifier is hydrogenated. In some embodiments the tackifier has a softening point (Ring and Ball, as measured by ASTM E-28) of 80° C. to 140° C., preferably 100° C. to 130° C. The tackifier, if present, is typically present at about 1 wt % to about 50 wt %, based upon the weight of the blend, more preferably 10 wt % to 40 wt %, even more preferably 20 wt % to 40 wt %.

In another embodiment, the functionalized (and optionally derivitized) polyolefins of this invention, and/or blends thereof, further comprise typical additives known in the art such as fillers, cavitating agents, antioxidants, surfactants, adjuvants, plasticizers, block, antiblock, color masterbatches, pigments, dyes, processing aids, UV stabilizers, neutralizers, lubricants, waxes, and/or nucleating agents. The additives may be present in the typically effective amounts well known in the art, such as 0.001 wt % to 10 wt %. Preferred fillers, cavitating agents and/or nucleating agents include titanium dioxide, calcium carbonate, barium sulfate, silica, silicon dioxide, carbon black, sand, glass beads, mineral aggregates, talc, clay and the like. Preferred antioxidants include phenolic antioxidants, such as Irganox 1010, Irganox, 1076 both available from Ciba-Geigy. Preferred oils include paraffinic or naphthenic oils such as Primol 352, or Primol 876 available from ExxonMobil Chemical France, S.A. in Paris, France. More preferred oils include aliphatic naphthenic oils, white oils or the like.

In a particularly preferred embodiment, the functionalized (and optionally derivitized) polyolefins produced herein are combined with polymers (elastomeric and/or thermoplastic) having functional groups such as unsaturated molecules-vinyl bonds, ketones or aldehydes under conditions such that they react. Reaction may be confirmed by an at least 20% (preferably at least 50%, preferably at least 100%) increase in Mw as compared to the Mw of the functionalized polyolefin prior to reaction. Such reaction conditions may be increased heat (for example, above the Tm of the functionalized polyolefin), increased shear (such as from a reactive extruder), presence or absence of solvent. Conditions useful for reaction include temperatures from 150° C. to 240° C. and where the components can be added to a stream comprising polymer and other species via a side arm extruder, gravimetric feeder, or liquids pump. Useful polymers having functional groups that can be reacted with the functionalized polyolefins produced herein include polyesters, polyvinyl acetates, nylons (polyamides), polybutadiene, nitrile rubber, hydroxylated nitrile rubber. In some embodiments, the functionalized (and optionally derivitized) polyolefin of this invention may be blended with up to 99 wt % (preferably up to 25 wt %, preferably up to 20 wt %, preferably up to 15 wt %, preferably up to 10 wt %, preferably up to 5 wt %), based upon the weight of the composition, of one or more additional polymers. Suitable polymers include those described as PM1) to PM 7) in U.S. Pat. No. 8,003,725.

Applications

The functionalized VTMs of this invention (and blends thereof as described above) may be used in any known thermoplastic or elastomer application. Examples include uses in molded parts, films, tapes, sheets, tubing, hose, sheeting, wire and cable coating, adhesives, shoe soles, bumpers, gaskets, bellows, films, fibers, elastic fibers, nonwovens, spun bonds, corrosion protection coatings and sealants. Preferred uses include additives for lubricants and/or fuels.

In some embodiments the functionalized vinyl terminated macromonomers produced herein are further functionalized (derivitized), such as described in U.S. Pat. No. 6,022,929; A. Toyota, T. Tsutsui, and N. Kashiwa, 48 POLYMER BULLETIN 213-219 (2002); 112 J. AM. CHEM. Soc. 7433-7434 (1990); and WO 2009/155472.

The functionalized vinyl terminated materials prepared herein may be used in oil additivition, lubricants, fuels and many other applications. Preferred uses include additives for lubricants and or fuels.

In particular embodiments herein, the vinyl terminated macromonomers disclosed herein, or functionalized/derivitized analogs thereof, are useful as additives, preferably in a lubricant.

The functionalized VTM's and/or derivitized VTM's produced herein have uses as lubricating additives which can act as dispersants, viscosity index improvers, or multifunctional viscosity index improvers. Additionally they may be used as disinfectants (functionalized amines) and or wetting agents.

Functionalized VTMs and/or derivitized VTMs having uses as dispersants typically have Mn's (g/mol) of less than 20,000, preferably less than 10,000 and most preferably less than 8,000 and typically can range from 500 to 10,000 (e.g. 500 to 5,000), preferably from 1,000 to 8,000 (e.g. 1,000 to 5,000) and most preferably from 1,500 to 6,000 (e.g. 1,500 to 3,000).

The functionalized VTMs and/or derivitized VTMs described herein having Mn's (g/mol) of greater than 10,000 g/mol, preferably greater than 10,000 to 100,000 g/mol (preferably 20,000 to 60,000 g/mol) are useful for viscosity index improvers for lubricating oil compositions, adhesive additives, antifogging and wetting agents, ink and paint adhesion promoters, coatings, tackifiers and sealants, and the like. In addition, such VTMs may be functionalized and derivitized to make multifunctional viscosity index improvers which also possess dispersant properties. (For more information please see U.S. Pat. No. 6,022,929.)

The functionalized VTMs and/or derivitized VTMs described herein may be combined with other additives (such as viscosity index improvers, corrosion inhibitor, oxidation inhibitor, dispersant, lube oil flow improver, detergents, demulsifiers, rust inhibitors, pour point depressant, anti-foaming agents, antiwear agents, seal swellant, friction modifiers, and the like (described for example in U.S. Pat. No. 6,022,929 at columns 60, line 42-column 78, line 54 and the references cited therein) to form compositions for many applications, including but not limited to lube oil additive packages, lube oils, and the like. Compositions containing these additives are typically are blended into a base oil in amounts which are effective to provide their normal attendant function. Representative effective amounts of such additives are illustrated as follows:

Compositions	(Typical) wt %*	(Preferred) wt %*
V.I. Improver	1-12	1-4
Corrosion Inhibitor	0.01-3	0.01-1.5
Oxidation Inhibitor	0.01-5	0.01-1.5
Dispersant	0.1-10	0.1-5
Lube Oil Flow Improver	0.01-2	0.01-1.5
Detergents and Rust inhibitors	0.01-6	0.01-3
Pour Point Depressant	0.01-1.5	0.01-1.5
Anti-Foaming Agents	0.001-0.1	0.001-0.01
Antiwear Agents	0.001-5	0.001-1.5
Seal Swellant	0.1-8	0.1-4
Friction Modifiers	0.01-3	0.01-1.5
Lubricating Base Oil	Balance	Balance

In the table above, wt %'s are based on active ingredient content of the additive, and/or upon the total weight of any additive-package, or formulation which will be the sum of the A.I. weight of each additive plus the weight of total oil or diluent.

When other additives are employed, it may be desirable, although not necessary, to prepare additive concentrates comprising concentrated solutions or dispersions of the subject additives of this invention (in concentrate amounts herein-

above described), together with one or more of said other additives (said concentrate when constituting an additive mixture being referred to herein as an additive-package) whereby several additives can be added simultaneously to the base oil to form the lubricating oil composition. Dissolution of the additive concentrate into the lubricating oil may be facilitated by solvents and by mixing accompanied with mild heating, but this is not essential. The subject functionalized or derivitized VTMs of the present invention can be added to small amounts of base oil or other compatible solvents along with other desirable additives to form additive-packages containing active ingredients in collective amounts of typically from about 2.5 to about 90%, and preferably from about 15 to about 75%, and most preferably from about 25 to about 60% by weight additives in the appropriate proportions with the remainder being base oil.

The final formulations may employ typically about 10 wt % of the additive-package with the remainder being base oil.

In another embodiment, the vinyl terminated polyolefins described herein can be use in any process, blend or product disclosed in WO 2009/155472 or U.S. Pat. No. 6,022,929, which are incorporated by reference herein.

In a preferred embodiment, this invention relates to a fuel comprising any VTM produced herein. In a preferred embodiment, this invention relates to a lubricant comprising any VTM produced herein.

Experimental

Product Characterization

Products were characterized by ^1H NMR and ^{13}C NMR as follows.

^1H NMR

Unless otherwise stated, ^1H NMR data was collected at either 25° C. or 120° C. (for purposes of the claims, 120° C. shall be used) in a 5 mm probe using a spectrometer with a ^1H frequency of at least 400 MHz. Data was recorded using a maximum pulse width of 45° and either a 1 or 2 second delay between pulses. Typical NMR solvents such as CDCl_3 , CD_2Cl_2 or C_6D_6 were purchased from Cambridge Isotope Laboratories and were used at ambient temperatures in collection of the NMR data.

^{13}C NMR

Unless otherwise stated, ^{13}C NMR data was collected at 120° C. using a spectrometer with a ^{13}C frequency of at least 100 MHz. A 90 degree pulse, an acquisition time adjusted to give a digital resolution between 0.1 and 0.12 Hz, at least a 2 second pulse acquisition delay time with continuous broadband proton decoupling using swept square wave modulation without gating was employed during the entire acquisition period. The spectra were acquired with time averaging to provide a signal to noise level adequate to measure the signals of interest. Samples were dissolved in tetrachloroethane- d_2 (TCE) for high temperature measurements. Other solvents such as CDCl_3 , CD_2Cl_2 , or C_6D_6 were used at ambient temperatures.

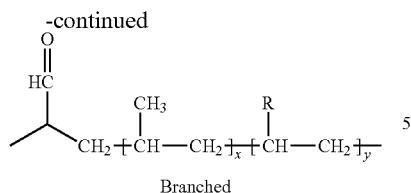
All molecular weights are g/mol unless otherwise noted.

Five different low molecular weight VTMs were selected for catalytic hydroformylation. The Vinyl Terminated Macromers used (Table 1) were made according to processes disclosed in U.S. Pat. Nos. 8,318,998 and/or 8,455,597, which are incorporated by reference in their entirety herein.

These initial tests were performed with $[\text{Rh}(\text{CO})_2\text{acac} + \text{PPh}_3]$ catalyst along with syngas. Run conditions are summarized in Table 1. The hydroformylated products contain two peaks between 1710-1735 cm^{-1} attributed to the carbonyl stretch and a peak at 2722 cm^{-1} attributed to the stretch from Polymer $-(\text{CO})-\text{H}$. All the products have distinctive ^1H NMR signatures associated with the introduced aldehyde group.

The presence of two aldehyde carbonyl stretches and two aldehyde carbon NMR resonances is attributed to the formation of two aldehyde products 1 and 2. Analytical data (Table 2) indicate conversion of vinyl chain end to aldehydes 1 and

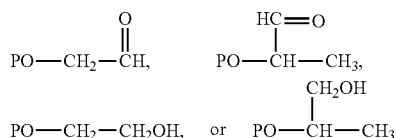
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All documents described herein are incorporated by reference herein, including any priority documents and/or testing procedures to the extent they are not inconsistent with this text, provided however that any priority document not named in the initially filed application or filing documents is NOT incorporated by reference herein. As is apparent from the foregoing general description and the specific embodiments, while forms of the invention have been illustrated and described, various modifications can be made without departing from the spirit and scope of the invention. Accordingly, it is not intended that the invention be limited thereby. Likewise, the term "comprising" is considered synonymous with the term "including" for purposes of Australian law. Likewise whenever a composition, an element or a group of elements is preceded with the transitional phrase "comprising", it is understood that we also contemplate the same composition or group of elements with transitional phrases "consisting essentially of," "consisting of," "selected from the group of consisting of," or "is" preceding the recitation of the composition, element, or elements and vice versa. Thus, the term "comprising" encompasses the terms "consisting essentially of," "is," and "consisting of and anyplace "comprising" is used "consisting essentially of," "is," or "consisting of" may be substituted therefor.

What is claimed is:

1. A polyolefin composition comprising one or more of the following formulae:



wherein the PO is the residual portion of a vinyl terminated macromonomer (VTM) having had a terminal unsaturated carbon of an allylic chain and a vinyl carbon adjacent to the terminal unsaturated carbon;

wherein the VTM is a vinyl terminated polymer has greater than 30% allyl chain ends relative to total unsaturations with an Mn of greater than 10,000 g/mol; and

wherein terminal aldehyde functionalized polyolefin to internal aldehyde functionalized product ratio is from about 60:40 to about 70:30 percent as measured by ¹H NMR.

2. A process to functionalize polyolefins comprising contacting a transition metal catalyst with carbon monoxide, in the presence of hydrogen, and one or more vinyl terminated macromonomers (VTMs) to provide polyolefins functionalized with an aldehyde group or a hydroxyl group; wherein terminal aldehyde functionalized polyolefin to internal aldehyde functionalized product ratio is from about 60:40 to about 70:30 percent as measured by ¹H NMR.

3. The process of claim 2, wherein the transition metal catalyst is a rhodium or a cobalt catalyst.

4. The process of claim 3, further comprising triphenyl phosphine.

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5. The process of claim 2, wherein the vinyl terminated macromonomer is one or more of:

(i) a vinyl terminated polymer having greater than 30% allyl chain ends relative to total unsaturations with an Mn or greater than 10,000;

(ii) a vinyl terminated polymer having an Mn of at least 160 g/mol;

(iii) a copolymer having an Mn of 300 g/mol or more (measured by ¹H NMR) comprising (a) from about 20 mol % to about 99.9 mol % of at least one C₅ to C₄₀ higher olefin, and (b) from about 0.1 mol % to about 80 mol % of propylene, wherein the higher olefin copolymer has at least 40% allyl chain ends relative to total unsaturations;

(iv) a copolymer having an Mn of 300 g/mol or more (measured by ¹H NMR), and comprises (a) from about 80 mol % to about 99.9 mol % of at least one C₄ olefin, (b) from about 0.1 mol % to about 20 mol % of propylene; and wherein the vinyl terminated macromonomer has at least 40% allyl chain ends relative to total unsaturation;

(v) a co-oligomer having an Mn of 300 g/mol to 30,000 g/mol (measured by ¹H NMR) comprising 10 mol % to 90 mol % propylene and 10 mol % to 90 mol % of ethylene, wherein the oligomer has at least X % allyl chain ends relative to total unsaturations, where: 1) X = (-0.94 * (mol % ethylene incorporated) + 100), when 10 mol % to 60 mol % ethylene is present in the co-oligomer, 2) X = 45, when greater than 60 mol % and less than 70 mol % ethylene is present in the co-oligomer, and 3) X = (1.83 * (mol % ethylene incorporated) - 83), when 70 mol % to 90 mol % ethylene is present in the co-oligomer;

(vi) a propylene oligomer, comprising more than 90 mol % propylene and less than 10 mol % ethylene wherein the oligomer has: at least 93% allyl chain ends relative to total unsaturations, a number average molecular weight (Mn) of about 500 g/mol to about 20,000 g/mol, an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.35:1.0, less than 100 ppm aluminum, and/or less than 250 regio defects per 10,000 monomer units;

(vii) a propylene oligomer, comprising: at least 50 mol % propylene and from 10 mol % to 50 mol % ethylene, wherein the oligomer has: at least 90% allyl chain ends relative to total unsaturations, an Mn of about 150 g/mol to about 20,000 g/mol, and an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.2:1.0, wherein monomers having four or more carbon atoms are present at from 0 mol % to 3 mol %;

(viii) a propylene oligomer, comprising: at least 50 mol % propylene, from 0.1 mol % to 45 mol % ethylene, and from 0.1 mol % to 5 mol % C₄ to C₁₂ olefin, wherein the oligomer has: at least 90% allyl chain ends relative to total unsaturations, an Mn of about 150 g/mol to about 10,000 g/mol, and an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.35:1.0;

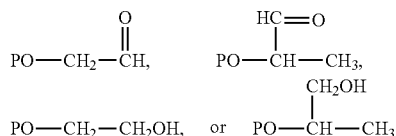
(ix) a propylene oligomer, comprising: at least 50 mol % propylene, from 0.1 mol % to 45 mol % ethylene, and from 0.1 mol % to 5 mol % diene, wherein the oligomer has: at least 90% allyl chain ends relative to total unsaturations, an Mn of about 150 g/mol to about 10,000 g/mol, and an isobutyl chain end to allylic vinyl group ratio of 0.7:1 to 1.35:1.0;

(x) a homo-oligomer, comprising propylene, wherein the oligomer has: at least 93% allyl chain ends relative to total unsaturations, an Mn of about 500 g/mol to about 70,000 g/mol, an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.2:1.0, and less than 1400 ppm aluminum;

(xi) vinyl terminated polyethylene having: (a) at least 60% allyl chain ends relative to total unsaturations; (b) a molecular weight distribution of less than or equal to

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- 4.0; (c) a $g'(\text{vis})$ of greater than 0.95; and (d) an Mn ($^1\text{H NMR}$) of at least 20,000 g/mol; and
- (xii) vinyl terminated polyethylene having: (a) at least 50% allyl chain ends relative to total unsaturations; (b) a molecular weight distribution of less than or equal to 4.0; (c) a $g'(\text{vis})$ of 0.95 or less; (d) an Mn ($^1\text{H NMR}$) of at least 7,000 g/mol; and (e) a Mn (GPC)/Mn ($^1\text{H NMR}$) in the range of from about 0.8 to about 1.2.
6. The process of claim 2, wherein the polyolefins functionalized with an aldehyde group or a hydroxyl group comprise:



wherein the PO is the residual portion of a vinyl terminated macromonomer (VTM) having had a terminal unsaturated carbon of an allylic chain and a vinyl carbon adjacent to the terminal unsaturated carbon.

7. The process of claim 2, wherein the polyolefins functionalized with an aldehyde group or a hydroxyl group are amorphous.

8. The process of claim 2, wherein the yield of terminal aldehyde functionalized polyolefin and internal aldehyde functionalized products is greater than 80 percent.

9. A reaction product of a vinyl terminated macromonomer (VTM) and carbon monoxide.

10. The reaction product of claim 9, wherein the VTM is one or more of:

- (i) a vinyl terminated polymer having greater than 30% allyl chain ends relative to total unsaturations with an Mn of greater than 10,000 g/mol;
- (ii) a vinyl terminated polymer having an Mn of at least 160 g/mol (measured by $^1\text{H NMR}$) comprising of one or more C_4 to C_{40} higher olefin derived units, where the higher olefin polymer comprises substantially no propylene derived units; and wherein the higher olefin polymer has at least 5% allyl chain ends relative to total unsaturations;
- (iii) a copolymer having an Mn of 300 g/mol or more (measured by $^1\text{H NMR}$) comprising (a) from about 20 mol % to about 99.9 mol % of at least one C_5 to C_{40} higher olefin, and (b) from about 0.1 mol % to about 80 mol % of propylene, wherein the higher olefin copolymer has at least 40% allyl chain ends relative to total unsaturations;
- (iv) a copolymer having an Mn of 300 g/mol or more (measured by $^1\text{H NMR}$), and comprises (a) from about 80 mol % to about 99.9 mol % of at least one C_4 olefin, (b) from about 0.1 mol % to about 20 mol % of propylene; and wherein the vinyl terminated macromonomer has at least 40% allyl chain ends relative to total unsaturation;
- (v) a co-oligomer having an Mn of 300 g/mol to 30,000 g/mol (measured by $^1\text{H NMR}$) comprising 10 mol % to 90 mol % propylene and 10 mol % to 90 mol % of ethylene, wherein the oligomer has at least X % allyl

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chain ends relative to total unsaturations, where: 1) $X = (-0.94 * (\text{mol \% ethylene incorporated}) + 100)$, when 10 mol % to 60 mol % ethylene is present in the co-oligomer, 2) $X = 45$, when greater than 60 mol % and less than 70 mol % ethylene is present in the co-oligomer, and 3) $X = (1.83 * (\text{mol \% ethylene incorporated}) - 83)$, when 70 mol % to 90 mol % ethylene is present in the co-oligomer;

(vi) a propylene oligomer, comprising more than 90 mol % propylene and less than 10 mol % ethylene wherein the oligomer has: at least 93% allyl chain ends relative to total unsaturations, a number average molecular weight (Mn) of about 500 g/mol to about 20,000 g/mol, an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.35:1.0, less than 100 ppm aluminum, and/or less than 250 regio defects per 10,000 monomer units;

(vii) a propylene oligomer, comprising: at least 50 mol % propylene and from 10 mol % to 50 mol % ethylene, wherein the oligomer has: at least 90% allyl chain ends relative to total unsaturations, an Mn of about 150 g/mol to about 20,000 g/mol, and an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.2:1.0, wherein monomers having four or more carbon atoms are present at from 0 mol % to 3 mol %;

(viii) a propylene oligomer, comprising: at least 50 mol % propylene, from 0.1 mol % to 45 mol % ethylene, and from 0.1 mol % to 5 mol % C_4 to C_{12} olefin, wherein the oligomer has: at least 90% allyl chain ends relative to total unsaturations, an Mn of about 150 g/mol to about 10,000 g/mol, and an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.35:1.0;

(ix) a propylene oligomer, comprising: at least 50 mol % propylene, from 0.1 mol % to 45 mol % ethylene, and from 0.1 mol % to 5 mol % diene, wherein the oligomer has: at least 90% allyl chain ends relative to total unsaturations, an Mn of about 150 g/mol to about 10,000 g/mol, and an isobutyl chain end to allylic vinyl group ratio of 0.7:1 to 1.35:1.0;

(x) a homo-oligomer, comprising propylene, wherein the oligomer has: at least 93% allyl chain ends relative to total unsaturations, an Mn of about 500 g/mol to about 70,000 g/mol, an isobutyl chain end to allylic vinyl group ratio of 0.8:1 to 1.2:1.0, and less than 1400 ppm aluminum;

(xi) vinyl terminated polyethylene having: (a) at least 60% allyl chain ends relative to total unsaturations; (b) a molecular weight distribution of less than or equal to 4.0; (c) a $g'(\text{vis})$ of greater than 0.95; and (d) an Mn ($^1\text{H NMR}$) of at least 20,000 g/mol; and

(xii) vinyl terminated polyethylene having: (a) at least 50% allyl chain ends relative to total unsaturations; (b) a molecular weight distribution of less than or equal to 4.0; (c) a $g'(\text{vis})$ of 0.95 or less; (d) an Mn ($^1\text{H NMR}$) of at least 7,000 g/mol; and (e) a Mn (GPC)/Mn ($^1\text{H NMR}$) in the range of from about 0.8 to about 1.2.

11. The process of any of claim 2, wherein the M_n is greater than or equal to 10,000 g/mol.

12. The reaction product of either of claim 9, wherein the M_n is greater than or equal to 10,000 g/mol.

13. The reaction product of claim 10, wherein the M_n is greater than or equal to 10,000 g/mol.

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